



Corso Luigi Einaudi, 55 - Torino

Appunti universitari

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# A P P U N T I

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MATERIA : Gasdinamica

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# GASDINAMICA

## TEORIA CINETICA E TERMODINAMICA

- LIBERO CAMMINO MEDIO: distanza media percorsa da una particella tra due urti  

$$P = \frac{1}{d^2 n \pi \sqrt{2}}$$
 dove  $d$  = diametro particelle  
 $n$  = numero di particelle;  $n = \frac{N_a}{V_{volume}}$

- VELOCITÀ  $V = \bar{V} + V'$  la velocità di un fluido è somma della sua velocità media d'insieme  $\bar{V}$  (velocità macroscopica) e da una fluttuazione locale dovuta all'agitazione termica  $V'$  (o  $V_{at}$ )

- VELOCITÀ DI AGITAZIONE TERMICA

$$V_{at} = \sqrt{2E_t \frac{1}{m}}$$

dove  $E_t$  = energia traslazionale media  
 $m$  = massa di gas coinvolto

- ENERGIA TRASLAZIONALE MEDIA

$$E_t = \frac{1}{2} m (\overline{U^2} + \overline{V^2} + \overline{W^2}) \quad E_{t, \text{caorico}} = \frac{1}{2} m (\overline{U^2} + \overline{V^2} + \overline{W^2})$$

- legame con la temperatura

$$E_t = \frac{3}{2} K_b T \quad \text{dove } K_b = 1,38 \cdot 10^{-23} \text{ J/KmolK}$$

costante di Boltzmann

- VELOCITÀ DEL SUONO

$$a = \sqrt{\gamma \frac{R}{M} T}$$

$R = K_b \cdot N_a = 8314 \text{ J/KmolK}$  = COSTANTE DEL GAS  
 $M = m \cdot N_a$  = MASSA MOLARE  
 $\gamma = C_p / C_v$

- IPOTESI DI FLUIDO CONTINUO

$Kn = \frac{\lambda}{L}$  n° di Knudsen; esprime il confronto tra il libero cammino medio e la lunghezza caratteristica del corpo

$Kn < 0,01$	FLUIDO CONTINUO
$Kn < 0,1$	SUP FLOW
$Kn < 10$	FLUIDO MODERATAMENTE RAREFATTO
$Kn > 10$	FLUIDO ALTAMENTE RAREFATTO

- EQUIDARTIZIONE DELL'ENERGIA

data una molecola con  $L$  gradi di libertà, l'energia complessiva  $E_L$  è data dalla somma delle energie spettanti a ogni singolo grad

$$E = \frac{1}{2} K_b T \quad E_L = \sum E = L \cdot \frac{1}{2} K_b T$$

- CALORI SPECIFICI

$$C_v = \left( \frac{dq}{dT} \right)_{V_{const}} = \left( \frac{dE}{dT} \right) = \frac{L}{2} \cdot \frac{R}{M} \quad C_v = \frac{\gamma}{\gamma-1} \cdot \frac{R}{M}$$

$$C_p = \left( \frac{dq}{dT} \right)_{P_{const}} = \left( \frac{dE}{dT} \right) = \frac{L+2}{2} \cdot \frac{R}{M} \quad C_p = \frac{1}{\gamma-1} \cdot \frac{R}{M}$$

dove  $\gamma = \frac{C_p}{C_v} = \frac{L+2}{L}$

$$R/M = C_p - C_v$$

- LEGGE DI BERNOLLI

$$dp = -pVdV \text{ (forma differenziale)} \rightarrow P_0 = P \cdot \frac{1}{2} PV^2 \text{ (caso incompressibile)}$$

$$\frac{dp}{dp} = -pV \frac{dV}{dp} = -a^2 \quad \text{dove } a = \text{velocità del suono}$$

e  $M = \frac{V}{a} = \text{n° di Mach}$  e  $a^2 = \left( \frac{\partial p}{\partial \rho} \right)$

$$\frac{dp}{p} = -M^2 \frac{dV}{V}$$

## FLUSSO DI ENERGIA

• LEGGE DI FOURIER:  $q_x = -\lambda \frac{\partial T}{\partial x}$  si ha un flusso di energia in presenza di un gradiente termico

• NUMERO DI PRANDTL

$$Pr = \frac{u C_p}{\lambda} = \frac{\nu}{K} \quad \text{dove } K = \frac{\lambda}{\rho C_p} \text{ è detta diffusività termica.}$$

$Pr = \frac{\text{DIFFUSIVITÀ VISCOSA}}{\text{DIFFUSIVITÀ TERMICA}}$ ,  $Pr$  indica anche il rapporto delle estensioni degli strati limite viscoso  $\delta$  e termico  $\delta_t$

• FORMULA DI EUCKEN

$$Pr = \frac{2L + 4}{2L + 9} = \frac{48}{98 - 5}$$

## FLUSSO DI MASSA

$$\bar{J}_x = -D \frac{ds}{dx} \rightarrow \text{LEGGE DI FICK}$$

il trasporto di massa avviene seguendo il gradiente di concentrazione di una certa specie  $S$ . ( $ds/dx =$  gradiente lungo  $x$ )

## TERMODINAMICA

• Eq. di STATO  $\rightarrow P \cdot V = n \cdot R/M \cdot T \rightarrow P \cdot V = N \cdot R \cdot T$

### 1° PRINCIPIO

$$de = \delta q + \delta L$$

• Sia il sistema considerato in equilibrio, se si fornisce calore o si compie lavoro, ce ne varia l'energia interna!

da cui:  $(\delta L)_{rev} = -p dv$ ,  $de = \delta q - p dv$

in forma entalpica

$$dh = \delta q + v dp$$

### 2° PRINCIPIO

$s =$  entropia per unità di massa (FUNZIONE DI STATO)

$$ds = \frac{dq}{T} + ds_{irrev.} \quad \text{dove } ds_{irrev.} \geq 0$$

A causa dei fenomeni dissipativi, tutti i processi avvengono a entropia crescente.

I-II

$$T ds = de + p dv$$

$$T ds = dh + v dp$$

da un punto di vista differenziale:  $T = \frac{Ds}{Df} = \frac{De}{Df} + p \frac{Dv}{Df}$

• CALCOLO DELL'ENTROPIA

$$ds = C_p \frac{dT}{T} - \frac{R}{M} \frac{dp}{p} \rightarrow s_2 - s_1 = C_p \ln\left(\frac{T_2}{T_1}\right) - \frac{R}{M} \ln\left(\frac{p_2}{p_1}\right)$$

$$ds = C_v \frac{dT}{T} - \frac{R}{M} \frac{dv}{v} \rightarrow s_2 - s_1 = C_v \ln\left(\frac{T_2}{T_1}\right) + \frac{R}{M} \ln\left(\frac{v_2}{v_1}\right)$$

EQ. DELL'ENTROPIA

• PROCESSI ISOENTROPICI

$$\frac{p_2}{p_1} = \left(\frac{T_2}{T_1}\right)^{\frac{\gamma}{\gamma-1}}; \quad \frac{p_2}{\rho_2} = \left(\frac{T_2}{T_1}\right)^{\frac{1}{\gamma-1}}; \quad \frac{p_2}{p_1} = \left(\frac{\rho_2}{\rho_1}\right)^{\gamma}; \quad \left(\frac{p}{\rho}\right)^{\frac{1}{\gamma}} = \text{cost.}$$

## RIPASSO SU OPERATORI

•  $\nabla = \frac{\partial}{\partial x} \bar{i} + \frac{\partial}{\partial y} \bar{j} + \frac{\partial}{\partial z} \bar{k}$

• Prodotto scalare:  $\bar{a} \cdot \bar{b} = a \cdot b \cos \alpha = a_x b_x + a_y b_y + a_z b_z$   
 $a \cdot a = |a|^2$

• Prodotto vettoriale:  $\bar{a} \times \bar{b} = a \cdot b \sin \alpha = (a_y b_z - a_z b_y) \bar{i} + \dots + \bar{k}$

• GRADIENTE  $\nabla \phi = \frac{\partial \phi}{\partial x} \bar{i} + \frac{\partial \phi}{\partial y} \bar{j} + \frac{\partial \phi}{\partial z} \bar{k}$  il gradiente di uno scalare è un vettore che indica la direzione in cui è MASSIMA LA VARIAZIONE DELLO SCALARE

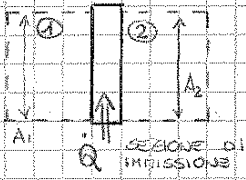
• DIVERGENZA  $\nabla \cdot \bar{V} = \frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} + \frac{\partial v_z}{\partial z}$  la divergenza di un vettore fornisce uno scalare che indica la tendenza del flusso a entrare / uscire

• ROTORE  $\nabla \times \bar{V} = \left( \frac{\partial v_z}{\partial y} - \frac{\partial v_y}{\partial z} \right) \bar{i} + \left( \frac{\partial v_x}{\partial z} - \frac{\partial v_z}{\partial x} \right) \bar{j} + \left( \frac{\partial v_y}{\partial x} - \frac{\partial v_x}{\partial y} \right) \bar{k}$

il rotore è legato alla velocità angolare  $\nabla \times \bar{V} = 2\bar{\omega} = 2\omega_x \bar{i} + 2\omega_y \bar{j} + 2\omega_z \bar{k}$

## FLUSSI UNIDIMENSIONALI 1D

SI CONSIDERA UN VOLUME DI CONTROLLO ARBITRARIO FISSO, INDEFORMABILE ED EUCLIDEANO. CONSIDERIAMO UN FLUSSO:



- STAZIONARIO ( $\partial/\partial t = 0$ )
- SENZA FORZE DI MASSA ( $F = 0$ )
- NON VISCOSO ( $\bar{V} = u\bar{i}$ )
- UNIFORME (PROPRIETA' COSTANTI LUNGO LA SEZ. TRASVERSALE)

PER LE IPOTESI FATE POSSO RISCRIVERE LE EQ. DI BILANCIO

- MASSA  $\rho_1 u_1 = \rho_2 u_2$
- Q.M  $\rho_1 + \rho_1 u_1^2 = \rho_2 + \rho_2 u_2^2$
- ENERGIA  $q + h_1 + \frac{u_1^2}{2} = h_2 + \frac{u_2^2}{2}$

## PROPAGAZIONE DI PICCOLE PERTURBAZIONI

LA PROPAGAZIONE DEL SUONO È UN PROCESSO ADIABATICO, REVERSIBILE → ISENTROPICO.

- dalla CONTINUITÀ ricavo  $a = -\rho \frac{da}{d\rho}$  } da cui ottengo:  $a = \left( \frac{dp}{d\rho} \right)_{\text{isotr.}} = \sqrt{\gamma \frac{p}{\rho}}$

- dalla Q.M  $\frac{da}{d\rho} = \frac{d(\gamma p)}{d\rho} + a^2$

OGGI LE PICCOLE PERTURBAZIONI ISENTROPICHE SI PROPAGANO ALLA VELOCITÀ DEL SUONO

## URTO RETTO



dato un pistone in un fluido con condizioni iniziali  $T_1, \rho_1, a_1$  uguali sia in I che in II. Supponiamo di imprimere al pistone un impulso infinitesimo  $du$ .

I:  $\rho_1 dt, \rho_1 + dt, V_I = a_1$   
 II:  $\rho_2 - dt, \rho_2 - dt, V_{II} = a_2$

Incrementando ancora la velocità si trova che

LE ONDE DI PERTURBAZIONE GENERATE AVRANNO VELOCITÀ:

$V_{I2} = \sqrt{\gamma \frac{p}{\rho}} \left( T_1 + dt \right) + du > a_1$

$V_{II2} = \sqrt{\gamma \frac{p}{\rho}} \left( T_1 + dt \right) - du < a_1$

LE ONDE DI ESPANSIONE SUCCESSIVE (II) SARANNO SEMPRE PIÙ LENTE E TENDERANNO A DISTANZIARSI, MENTRE LE ONDE DI COMPRESSIONE (I) RISULTANO PIÙ VELOCI E TENDONO AD INTRACCIETARSI IN UN URTO

# FLUSSO DI RAYLEIGH

CAMPO 1D

$q \neq 0 \rightarrow$  scambio di calore  
 $T_v = 0 \rightarrow$  No attriti.

- EQUAZIONI:
- ① - CONTINUITÀ
  - ② - QDM
  - ③ - ENERGIA
  - ④ -  $\frac{p}{\rho} = \frac{R}{M} T$

$$\begin{aligned} \rho u_1 &= \rho_2 u_2 \\ \rho_1 + \rho_1 u_1^2 &= \rho_2 + \rho_2 u_2^2 \\ q + H_1 &= H_2 \end{aligned}$$

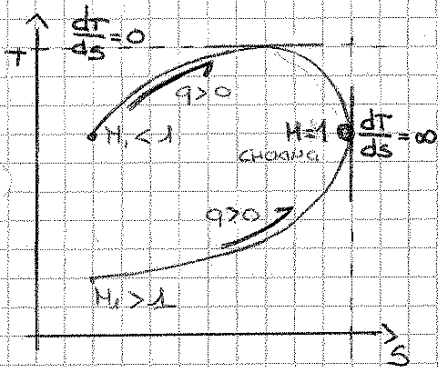
Si assegnano le condizioni nel campo I, si fornisce calore  $q$ .  
 Vogliamo valutare le condizioni nel campo II

da ①,  $H^0 = c_p \cdot T^0 \rightarrow H_1^0 + q = H_2^0 \rightarrow T_2^0 = T_1^0 + \frac{q}{c_p}$

da ②,  $\rho u^2 = \rho a^2 M^2 = \gamma p M^2 \rightarrow \rho_1 + \gamma p_1 M_1^2 = \rho_2 + \gamma p_2 M_2^2 \rightarrow \frac{\rho_2}{\rho_1} = \frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}$

è comodo  $\frac{\rho_2}{\rho_1} = \frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}$ ;  $\frac{p_2}{p_1} = \frac{1 + \frac{\gamma-1}{2} M_1^2}{1 + \frac{\gamma-1}{2} M_2^2} \cdot \left(\frac{M_1}{M_2}\right)^2$ ;  $\frac{T_2}{T_1} = \frac{(1 + \gamma M_1^2)}{(1 + \gamma M_2^2)} \cdot \left(\frac{M_1}{M_2}\right)^2$

$$S_2 - S_1 = c_p \ln \left[ \frac{1 + \gamma M_1^2}{1 + \gamma M_2^2} \cdot \left(\frac{M_1}{M_2}\right)^2 \right] - \frac{R}{M} \ln \left[ \frac{1 + \gamma M_1^2}{1 + \gamma M_2^2} \right]$$



$$\frac{dT}{ds} = c_v \cdot T \cdot \frac{(\gamma M^2 - 1)}{(M^2 - 1) \gamma}$$

$$\frac{dM}{ds} = \frac{c_v M}{\gamma (M^2 - 1)}$$

• INGRESSO SUBSONICO  $M_1^2 < 1$

$\frac{dT}{ds} > 0$  se  $\gamma M_1^2 - 1 < 0 \Rightarrow M_1 < \frac{1}{\sqrt{\gamma}} = 0,85$

$\frac{dT}{ds} < 0$  se  $\gamma M_1^2 - 1 > 0 \Rightarrow M_1 > \frac{1}{\sqrt{\gamma}} = 0,85$

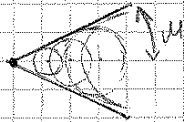
$\frac{dM}{ds} > 0$  FORNENDO CALORE LA VELOCITÀ AUMENTA (M crescente)

• INGRESSO SUPERSONICO  $M_1^2 > 1$

$\frac{dT}{ds} > 0$   $\frac{dM}{ds} < 0$  FORNENDO CALORE IL FLUSSO RALLENTA PORTANDOSI A  $M=1$

# ONDE OBLIQUE IN FLUSSI SUPERSONICI

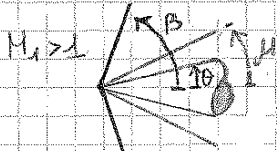
STUDIAMO UNA SORGENTE SONORA IN MOVIMENTO CON  $v_s > a$



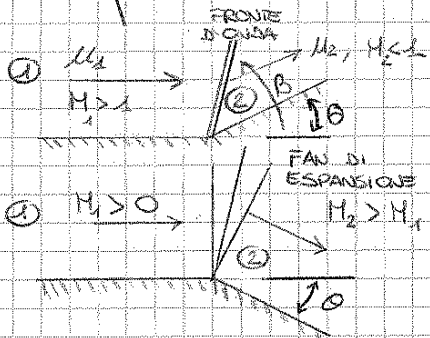
LE LINEE INDIVIDUATE DAL FRONTE D'ONDA PRENDONO IL NOME DI LINEE DI MACH, E FORMANO IL CONO DI MACH.  $M =$  SEMIAPERTURA DEL CONO DI MACH

PER LE PICCOLE PERTURBAZIONI, IL PROCESSO E' ISOENTROPICO  $\Rightarrow T_1^0 = T_2^0, P_1^0 = P_2^0$

## GRANDI PERTURBAZIONI



dove  $\theta =$  Semiapertura del cono  
 $M =$  " " del cono di MACH  
 $\beta =$  " " del cono di URTO



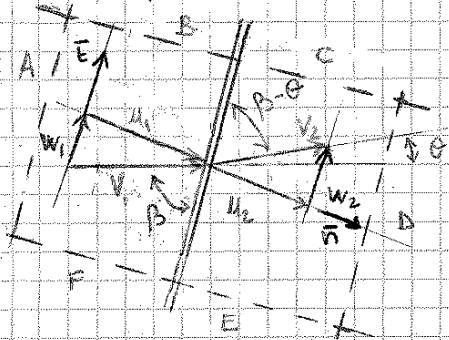
CAMPO ①  
 • uniforme  
 • parallelo alla parete

CAMPO ②  
 • uniforme  
 • deflesso di  $\theta$   
 • PARALLELO ALLA PARETE

- occorre ripetere la CONDIZIONE DI TANGENZIALITÀ

COMPRESSIONE  $\Rightarrow M_2 < M_1, P_2 > P_1, \rho_2 > \rho_1, T_2 > T_1$   
 ESPANSIONE  $\Rightarrow M_2 > M_1, P_2 < P_1, \rho_2 < \rho_1, T_2 < T_1$

## EQUAZIONI DELL'URTO OBLIQUO



$$\vec{V}_1 = M_1 \vec{W}_1$$

$$\vec{V}_2 = M_2 \vec{W}_2$$

- FLUSSO 2D ( $V = u\vec{n} + w\vec{e}$ )
- " " STAZIONARIO
- " " INVISCIDATO
- " " ADIABATICO

ADOTTO IL VOLUME DI CONTROLLO ABCDEF

- CONTINUITÀ  $\int_S \rho(\vec{V} \cdot \vec{n}) d\sigma \Rightarrow \rho_1 M_1 = \rho_2 M_2$

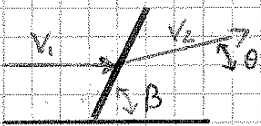
- Q.D.M. direzione NORMALE (N)  $\Rightarrow P_1 + \rho_1 M_1^2 = P_2 + \rho_2 M_2^2$

direzione TANGENZIALE (T)  $\Rightarrow \rho_1 M_1 W_1 = \rho_2 M_2 W_2 \Rightarrow W_1 = W_2$

- ENERGIA:  $h_1 + \frac{M_1^2}{2} = h_2 + \frac{M_2^2}{2}$

## URTO OBLIQUO

$\theta =$  deflessione della corrente  
 $\beta =$  inclinazione dell'urto



$$M_{1N} = \frac{M_1}{\sin \beta} = \frac{V_1 \sin \beta}{a_1} = M_1 \sin \beta$$

considero solo la direz. N  
 poiché per T,  $W_1 = W_2$

$$\frac{P_2}{P_1} = 1 + \frac{2\gamma}{\gamma-1} \left[ M_1^2 \sin^2 \beta - 1 \right] \quad e \quad \frac{P_2}{P_1} = \frac{M_1}{M_2} = \frac{(\gamma+1) M_1^2 \sin^2 \beta}{2 + (\gamma-1) M_1^2 \sin^2 \beta} \quad e \quad \frac{T_2}{T_1} = \frac{P_2}{P_1} \frac{\rho_1}{\rho_2}$$

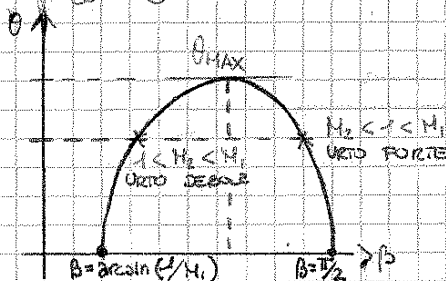
$$M_2 < M_1, \quad M_2 = \frac{1}{\sin(\beta-\theta)} \frac{1}{\frac{2 + (\gamma-1) M_1^2 \sin^2 \beta}{2\gamma M_1^2 \sin^2 \beta - (\gamma-1)}}$$

• A MONTE  $\tan(\beta) = M_1/W_1$   
 • A VALLE  $\tan(\beta-\theta) = M_2/W_2$

$$\rightarrow \frac{\tan(\beta-\theta)}{\tan(\beta)} = \frac{M_2}{M_1} \frac{P_1}{P_2} = \frac{2 + (\gamma-1) M_1^2 \sin^2 \beta}{(\gamma+1) M_1^2 \sin^2 \beta}$$

ricaviamo  $\theta$  con alcuni passaggi trigonometrici

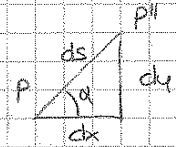
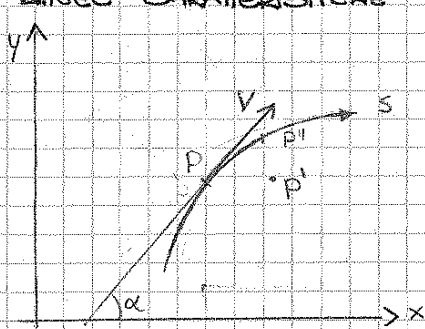
$$\tan \theta = \frac{2}{\tan \beta} \left[ \frac{M_1^2 \sin^2 \beta - 1}{M_1^2 (\gamma + \cos 2\beta) + 2} \right]$$



dato un qualunque valore  $\theta < \theta_{max}$  sono possibili 2 casi. La scelta tra urto forte e urto debole è funzione della pressione a valle.

PER  $\theta > \theta_{max}$  HO UN URTO CURVO, FORTE ALLA BASE CHE DIMINUISCE VERSO L'ESTERNO.

**LINEE CARATTERISTICHE**



$\frac{dy}{dx} = m = \tan \alpha$  pendenza di S nota.

V velocità punti di S  $(u^2 + v^2) = \bar{V}$

Supponendo il flusso irrotazionale:

$\frac{\partial u}{\partial x} = \frac{\partial^2 \phi}{\partial x^2}$ ,  $\frac{\partial v}{\partial y} = \frac{\partial^2 \phi}{\partial y^2}$ ,  $\frac{\partial u}{\partial y} = \frac{\partial v}{\partial x} = \frac{\partial^2 \phi}{\partial x \partial y}$

$u(P) = u(P) + \frac{\partial u}{\partial x} dx + \frac{\partial u}{\partial y} dy$

$v(P) = v(P) + \frac{\partial v}{\partial x} dx + \frac{\partial v}{\partial y} dy$

$\frac{dx}{ds} = \cos \alpha$ ,  $\frac{dy}{ds} = \sin \alpha$

$A_x = \frac{du}{ds} = \frac{\partial u}{\partial x} \frac{dx}{ds} + \frac{\partial u}{\partial y} \frac{dy}{ds}$  ;  $B_x = \frac{A_x}{\cos \alpha} = \frac{\partial^2 \phi}{\partial x^2} + m \frac{\partial^2 \phi}{\partial x \partial y}$

$A_y = \frac{dv}{ds} = \frac{\partial v}{\partial x} \frac{dx}{ds} + \frac{\partial v}{\partial y} \frac{dy}{ds}$  ;  $B_y = \frac{A_y}{\cos \alpha} = \frac{\partial^2 \phi}{\partial x \partial y} + m \frac{\partial^2 \phi}{\partial y^2}$

Eq. del potenziale per velocità

dove:  $H = \left(\frac{u^2}{a^2} - 1\right)$ ,  $L = \left(\frac{v^2}{a^2} - 1\right)$ ,  $2K = \frac{2uv}{a^2}$

risolvendo il sistema trova la velocità in ogni punto dell'intorno di S. IL SISTEMA NON HA SOLUZIONE se  $L - 2Km - Hm^2 = 0$ , ossia quando la tangente al punto P ha tangente  $\tan \mu$ , ossia è DIREZIONE CARATTERISTICA. SE LA TANGENTE È SEMPRE DIREZIONE CARATTERISTICA, LA LINEA S SI DICE LINEA CARATTERISTICA.

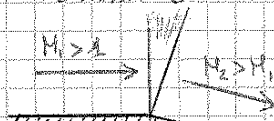
$\Delta = M^2 - 1 \rightarrow$  discriminante dell'equazione

- Se la corrente è supersonica ( $M^2 > 1$ ),  $\Delta > 0$ , l'equazione ammette due soluzioni, pertanto V saranno **DE** DIREZIONI CARATTERISTICHE le cui tangenti sono inclinate di un angolo  $\pm \mu = \arcsin(1/M)$
- In caso di correnteonica ( $M=1$ ) ho un'unica soluzione, con  $\mu=90^\circ$
- Per correnti subsoniche ( $M^2 < 1$ ) l'equazione non ammette soluzioni e conseguentemente nemmeno 0 direzioni caratteristiche.

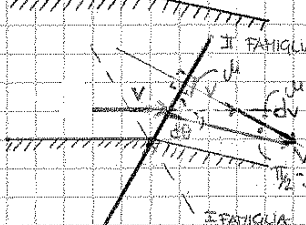
**RELAZIONE FONDAMENTALE:**

**ESPANSIONE ISENTROPICA**

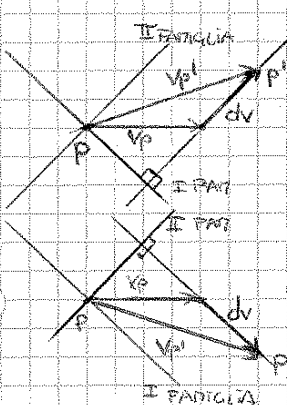
$d\theta = \pm \sqrt{M^2 - 1} \cdot \frac{dv}{v}$



Nel caso dell'espansione per piccole deflessioni, si ha che la variazione dv è ortogonale alla direzione caratteristica della II famiglia.



Se la deviazione fosse opposta sarebbe ortogonale alla direzione della I famiglia.



Voglio  $\frac{dv}{v} f\left(\frac{d\theta}{M}\right) \rightarrow \frac{dv}{v} = \frac{dM}{M} \frac{da}{a}$

$\frac{da}{a} : \left(\frac{a^2}{a}\right) = \frac{T^0}{T} = \left(1 + \frac{\gamma-1}{2} M^2\right) \rightarrow a = a_0 \cdot \left(1 + \frac{\gamma-1}{2} M^2\right)^{-1/2}$

$da = a_0 \cdot \left[-\frac{1}{2} \left(1 + \frac{\gamma-1}{2} M^2\right)^{-3/2} \cdot (\gamma-1) M dM\right]$

$\frac{da}{a} = -\left(\frac{\gamma-1}{2}\right) \left(1 + \frac{\gamma-1}{2} M^2\right)^{-1} M dM$

$\frac{dv}{v} = \frac{dM}{M} \cdot \left(\frac{1}{1 + \frac{\gamma-1}{2} M^2}\right) \rightarrow d\theta = \pm \frac{\sqrt{M^2-1}}{\left(1 + \frac{\gamma-1}{2} M^2\right)} \frac{dM}{M}$

INTEGRANDO OTTENGIO LA DEFLESSIONE  $\theta(M)$

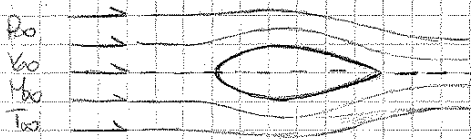
$\theta(M) = \theta + \text{cost} = \left[ \sqrt{\frac{\gamma-1}{\gamma+1}} \arctg\left(\sqrt{\frac{\gamma-1}{\gamma+1}} \sqrt{M^2-1}\right) - \arctg(\sqrt{M^2-1}) \right]$

CHE RAPPRESENTA LA FUNZIONE PER UN EPICICLOIDE



# TEORIA DELLE PICCOLE PERTURBAZIONI

È UNA TEORIA LINEARIZZATA PER FLUSSI SUPERSONICI O SUBSONICI COMPRESSIBILI. L'ipotesi di piccole perturbazioni permette di linearizzare e quindi semplificare il problema.



$$\vec{V} = V_x \hat{i} + V_y \hat{j} + V_z \hat{k}$$

A MONTE  $\begin{cases} V_x = V_{\infty} \\ V_y = 0 \\ V_z = 0 \end{cases}$  A VALLE  $\begin{cases} V_x = V_{\infty} + u' \\ V_y = v' \\ V_z = w' \end{cases}$

LA VELOCITÀ È SOTTOBIA A DEPRESSIONE E VALICAZIONE DEL MODO.

**IPOTESI:**

- PROFILO SOTTILE (Valida per 2D e corpi assialsimmetrici snelli e 3D)
- BASSA INCIDENZA
- FLUSSO ROTAZIONALE E INVISCIDO

$\Phi$  = FUNZIONE POTENZIALE DI PERTURBAZIONE.

$$u' = \frac{\partial \Phi}{\partial x} \quad v' = \frac{\partial \Phi}{\partial y} \quad w' = \frac{\partial \Phi}{\partial z}$$

$\bar{\Phi}$  = POTENZIALE TOTALE

$$\begin{cases} V_x = V_{\infty} + u' = \frac{\partial \bar{\Phi}}{\partial x} = V_{\infty} + \frac{\partial \Phi}{\partial x} \\ V_y = \frac{\partial \bar{\Phi}}{\partial y} = \frac{\partial \Phi}{\partial y} = v' \\ V_z = \frac{\partial \bar{\Phi}}{\partial z} = \frac{\partial \Phi}{\partial z} = w' \end{cases}$$

$$\left(1 - \frac{V_{\infty}^2}{a^2}\right) \bar{\Phi}_{xx} + \left(1 - \frac{V_{\infty}^2}{a^2}\right) \bar{\Phi}_{yy} + \left(1 - \frac{V_{\infty}^2}{a^2}\right) \bar{\Phi}_{zz} - 2 \frac{V_{\infty}}{a^2} \frac{\partial \bar{\Phi}}{\partial x} \frac{\partial \bar{\Phi}}{\partial y} - 2 \frac{V_{\infty}}{a^2} \frac{\partial \bar{\Phi}}{\partial x} \frac{\partial \bar{\Phi}}{\partial z} - 2 \frac{\partial \bar{\Phi}}{\partial y} \frac{\partial \bar{\Phi}}{\partial z} \bar{\Phi}_{xyz} = 0$$

SOSTITUENDO:

$$\left[a^2 - \left(V_{\infty} + \frac{\partial \Phi}{\partial x}\right)^2\right] \Phi_{xx} + \left[a^2 - \left(\frac{\partial \Phi}{\partial y}\right)^2\right] \Phi_{yy} + \left[a^2 - \left(\frac{\partial \Phi}{\partial z}\right)^2\right] \Phi_{zz} - 2 \left[V_{\infty} + \frac{\partial \Phi}{\partial x}\right] \frac{\partial \Phi}{\partial y} \frac{\partial \Phi}{\partial z} - 2 \left[V_{\infty} + \frac{\partial \Phi}{\partial x}\right] \frac{\partial \Phi}{\partial z} \frac{\partial \Phi}{\partial y} - 2 \left(\frac{\partial \Phi}{\partial y} \frac{\partial \Phi}{\partial z}\right) \frac{\partial \Phi}{\partial x} = 0$$

DETA. FUNZIONE POTENZIALE DI PERTURBAZIONE

INFORME COMP.

$$\left[a^2 - (V_{\infty} + u')^2\right] \frac{\partial u'}{\partial x} + \left[a^2 - v'^2\right] \frac{\partial v'}{\partial y} + \left[a^2 - w'^2\right] \frac{\partial w'}{\partial z} - 2(V_{\infty} + u')v' \frac{\partial u'}{\partial y} - 2(V_{\infty} + u')w' \frac{\partial u'}{\partial z} - 2v'w' \frac{\partial u'}{\partial x} = 0$$

ESPLICITO  $a^2$  IN FUNZIONE

DELLA VELOCITÀ DI PERTURBAZIONE

$$h_{\infty} + \frac{V_{\infty}^2}{2} = h + \frac{V^2}{2}$$

$$\frac{a^2}{\gamma - 1} + \frac{V_{\infty}^2}{2} = \frac{a^2}{\gamma - 1} + \frac{(V_{\infty} + u')^2 + v'^2 + w'^2}{2} \Rightarrow a^2 = a_{\infty}^2 - \frac{\gamma - 1}{2} \cdot (2u'V_{\infty} + u'^2 + v'^2 + w'^2)$$

E SOSTITUISCO NEGLI EQ. DI POTENZIALE:

$$\begin{aligned} (1 - M_{\infty}^2) \frac{\partial u'}{\partial x} + \frac{\partial v'}{\partial y} + \frac{\partial w'}{\partial z} &= M_{\infty}^2 \left[ \frac{u'}{V_{\infty}} + \frac{\gamma - 1}{2} \frac{u'^2}{V_{\infty}^2} + \frac{\gamma - 1}{2} \frac{(v'^2 + w'^2)}{V_{\infty}^2} \right] \frac{\partial u'}{\partial x} + D_1 \\ &+ M_{\infty}^2 \left[ (\gamma - 1) \frac{u'v'}{V_{\infty}^2} + \frac{\gamma - 1}{2} \frac{v'^2}{V_{\infty}^2} + \frac{\gamma - 1}{2} \frac{(u'w' + w'^2)}{V_{\infty}^2} \right] \frac{\partial v'}{\partial y} + D_2 \\ &+ M_{\infty}^2 \left[ (\gamma - 1) \frac{u'w'}{V_{\infty}^2} + \frac{\gamma - 1}{2} \frac{w'^2}{V_{\infty}^2} + \frac{\gamma - 1}{2} \frac{(u'v' + v'^2)}{V_{\infty}^2} \right] \frac{\partial w'}{\partial z} + D_3 \\ &+ M_{\infty}^2 \left[ \frac{v'w'}{V_{\infty}^2} \left(1 + \frac{u'}{V_{\infty}}\right) \left(\frac{\partial u'}{\partial y} + \frac{\partial v'}{\partial x}\right) + \frac{w'v'}{V_{\infty}^2} \left(1 + \frac{u'}{V_{\infty}}\right) \left(\frac{\partial u'}{\partial z} + \frac{\partial w'}{\partial x}\right) + \frac{v'w'}{V_{\infty}^2} \left(\frac{\partial v'}{\partial z} + \frac{\partial w'}{\partial y}\right) \right] + D_4 \end{aligned}$$

L'EQUAZIONE È ANCORA LEGATA (E NON LINEARE). PUÒ ESSERE APPLICATA SIA A FLUSSI INCOMPRESSIBILI CHE COMPRESSIBILI.

• ASSUNZIONI PER PICCOLE PERTURBAZIONI:  $\frac{u'}{V_{\infty}}, \frac{v'}{V_{\infty}}, \frac{w'}{V_{\infty}} \ll 1, \frac{u'^2}{V_{\infty}^2}, \frac{v'^2}{V_{\infty}^2} + \frac{w'^2}{V_{\infty}^2} \ll \ll 1$

PER  $0.8 \leq M_{\infty} \leq 0.9$   $\wedge$   $1.2 \leq M_{\infty} \leq 5$

EQ. POTENZIALE DELLE VELOCITÀ  $(1 - M_{\infty}^2) \frac{\partial u'}{\partial x} + \frac{\partial v'}{\partial y} + \frac{\partial w'}{\partial z} = 0$

$D_1 \ll (1 - M_{\infty}^2)$   
 $D_2, D_3, D_4 \ll 1$

la linearizzazione non è più accettabile in regime ipersonico, mentre non è possibile a causa degli urti in regimi transonici.

•  $C_p$  per flusso

$$C_p = \frac{p - p_{\infty}}{\frac{1}{2} \rho_{\infty} V_{\infty}^2} = \frac{2}{\gamma M_{\infty}^2} \left( \frac{p}{p_{\infty}} - 1 \right)$$

circa  $p/p_{\infty}$

$$T - T_{\infty} = \frac{V_{\infty}^2 - V^2}{2c_p} \quad \text{con} \quad c_p = \frac{\gamma}{\gamma - 1} \frac{R}{M} \Rightarrow \frac{T}{T_{\infty}} = 1 - \frac{\gamma - 1}{2 \gamma M_{\infty}^2} (2u'V_{\infty} + u'^2 + v'^2 + w'^2) \Rightarrow \frac{p}{p_{\infty}} = \left(\frac{T}{T_{\infty}}\right)^{\frac{\gamma}{\gamma - 1}} = 1 - (\dots)^{\frac{\gamma}{\gamma - 1}}$$

espando  $p/p_{\infty}$  in serie binomiale

$$\frac{p}{p_{\infty}} = 1 - \frac{\gamma}{2} M_{\infty}^2 \left( \frac{2u'V_{\infty}}{V_{\infty}^2} + \frac{u'^2 + v'^2 + w'^2}{V_{\infty}^2} \right) \Rightarrow C_p = - \frac{2u'}{V_{\infty}} - \frac{u'^2 + v'^2 + w'^2}{V_{\infty}^2}$$

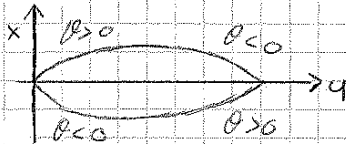
$$(1 - \epsilon)^{\alpha} = 1 - \alpha \epsilon$$

= 0 PER PICCOLE PERT.

# TEORIA DELLE PICCOLE PERTURBAZIONI IN SUPERSONICO

tiene conto di compressioni, espansioni e URTI.

Ricordando la TEORIA LINEARIZZATA:



$C_p = \frac{C_p}{\sqrt{1-M_\infty^2}}$

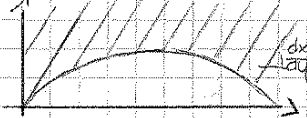
Subsonico:  $\beta^2 \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} = 0$ ;  $\beta = \sqrt{1-M_\infty^2}$

Supersonico:  $\lambda^2 \frac{\partial^2 \phi}{\partial x^2} = \frac{\partial^2 \phi}{\partial y^2} = 0$ ;  $\lambda = \sqrt{M_\infty^2 - 1}$

Cerca la funzione potenziale di perturbazione, assegnata la geometria

In generale:  $\lambda^2 \frac{\partial^2 \phi}{\partial x^2} - \frac{\partial^2 \phi}{\partial y^2} = 0$  è l'eq di un'onda, con soluzioni  $\phi = f(x-\lambda y) + g(x+\lambda y)$   
trovo quindi le soluzioni per  $y > 0$  e  $y < 0$

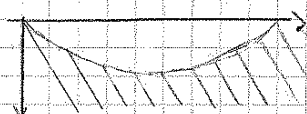
• DORSO ( $y \geq 0$ )  $\rightarrow \phi = f(x-\lambda y)$



le linee a  $\phi = \text{costante}$  individuano LINEE CARATTERISTICHE

$\frac{dx}{dy} = \tan(\theta) = \frac{1}{\sqrt{M_\infty^2 - 1}} = \frac{1}{\lambda}$

• VENTRE ( $y \leq 0$ )  $\rightarrow \phi = g(x+\lambda y)$



anche in questo caso le linee a  $\phi = \text{cost.}$  sono LINEE CARATTERISTICHE

$\frac{dx}{dy} = \tan(\theta) = -\frac{1}{\sqrt{M_\infty^2 - 1}} = -\frac{1}{\lambda}$

• CONDIZIONE DI TANGENZA (LINEARIZZATA)

occorre imporre la condizione di tangenza del flusso attorno al profilo



$\tan(\theta) = \frac{v'}{V_\infty + u'}$

DEVO ESPRIMERLA IN FUNZIONE DEL POTENZIALE SA PER IL DORSO CHE PER IL VENTRE

- DORSO  $u' = \frac{\partial \phi(x-\lambda y)}{\partial(x-\lambda y)} \cdot \frac{\partial(x-\lambda y)}{\partial x} = f'$   
 $v' = \frac{\partial \phi(x-\lambda y)}{\partial(x-\lambda y)} \cdot \frac{\partial(x-\lambda y)}{\partial y} = f'(-\lambda)$

- VENTRE  $u' = \frac{\partial \phi(x+\lambda y)}{\partial(x+\lambda y)} \cdot \frac{\partial(x+\lambda y)}{\partial x} = g'$   
 $v' = \frac{\partial \phi(x+\lambda y)}{\partial(x+\lambda y)} \cdot \frac{\partial(x+\lambda y)}{\partial y} = g'(\lambda)$

$f' = u'$ ,  $f' = -\frac{v'}{\lambda} \rightarrow u' = -\frac{v'}{\lambda}$

$g' = u'$ ,  $g' = \frac{v'}{\lambda}$ ,  $u' = \frac{v'}{\lambda}$

$\tan \theta = \frac{v'}{V_\infty + u'} \xrightarrow{u' \ll V_\infty, \tan \theta \approx \theta} V' = V_\infty \theta$

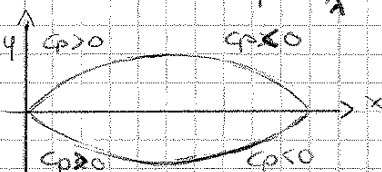
$\rightarrow V' = V_\infty \theta$

da cui:  $u' = \frac{V_\infty \theta}{\lambda} (-1)$

da cui:  $u' = \frac{V_\infty \theta}{\lambda}$

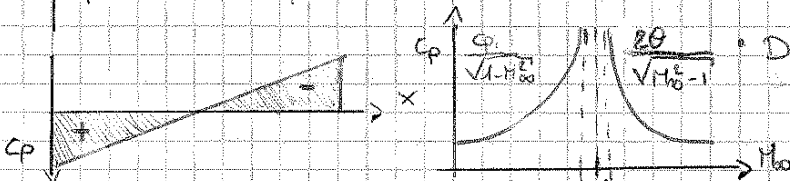
$C_p = \frac{2\theta}{\lambda}$

$C_p = -\frac{2\theta}{\lambda}$

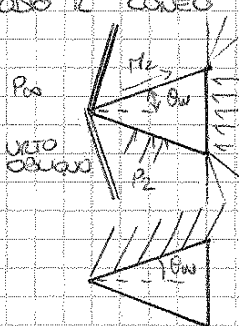


$C_p = \frac{p - p_\infty}{\frac{1}{2} \rho_\infty V_\infty^2}$

- deflessione nota data dalla geometria
- fluido non viscoso
- $\alpha = 0$
- $L = 0$  se il profilo è simmetrico, i contributi sono uguali
- $D \neq 0 \rightarrow$  RESISTENZA DI ONDA



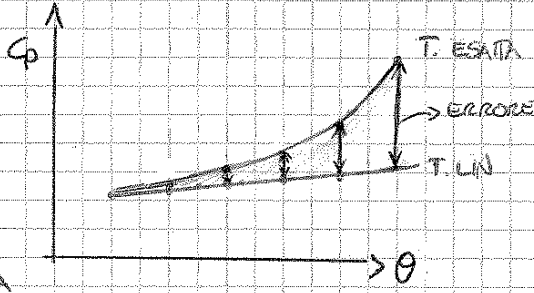
• CHE ERRORE SI COMMETTE CON LA TEORIA LINEARIZZATA? STUO IL CUCEO



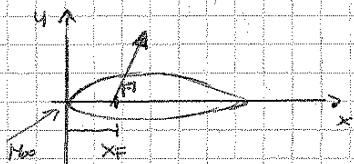
FAN DI ESPANSIONE

TEORIA ESATTA

TEORIA LINEARIZZATA



## PROPRIETA' FOCALI

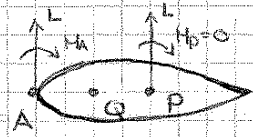


IL FUOCO DI UN PROFILO E' UN PUNTO CARATTERISTICO PER CUI IL MOMENTO MF E' COSTANTE

• PER UN FLUIDO INCOMPRESSIBILE  $X_f = 0,25 \cdot c$

$$C_{MA} = -\frac{2\alpha}{\sqrt{M_{\infty}^2 - 1}} - \frac{2}{\sqrt{M_{\infty}^2 - 1}} \frac{(S_u - S_l)}{c^2}$$

SIA P IL CENTRO DI PRESSIONE DEL PROFILO, CON  $X_{cp}$  NOTO



$$M_p = L \cdot (X_p - X_{cp}) = 0$$

$$M_A = -L X_{cp}$$

$$M_q = M_A + L X_q = M_p - L (X_p - X_{cp})$$

$$M_p = 0$$

$$M_A = -L X_{cp}$$

$$X_{cp} = -M_A / L$$

$$\frac{X_{cp}}{c} = \frac{C_{MA}}{C_L}$$

CONSIDERIAMO IL PUNTO O IL FUOCO DELL'ALA, SE  $P=O$ ,  $M_O = M_A + L X_O \rightarrow C_{M_O} = C_{MA} + C_L \cdot \frac{X_O}{c}$

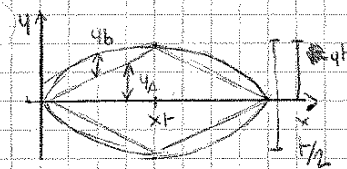
$$C_{M_O} = \left[ -\frac{2\alpha}{\sqrt{M_{\infty}^2 - 1}} - \frac{2}{\sqrt{M_{\infty}^2 - 1}} \frac{(S_u + S_l)}{c^2} \right] + \frac{4\alpha}{\sqrt{M_{\infty}^2 - 1}} \cdot \frac{X_O}{c}; \text{ PER LA PROPRIETA' FOCAL E' } \frac{\partial C_{M_O}}{\partial \alpha} = 0$$

$$\frac{\partial C_{M_O}}{\partial \alpha} = \frac{2}{\sqrt{M_{\infty}^2 - 1}} + \frac{4}{\sqrt{M_{\infty}^2 - 1}} \cdot \frac{X_O}{c} = 0 \rightarrow \frac{X_O}{c} = \frac{1}{2}$$

NEL SUPERSONICO IL FUOCO E' POSIZIONATO A META' DEL PROFILO

• DATI  $\alpha=0$ , spessore  $t$ , CERCO LA FORMA CON MINIMA RESISTENZA

- scompongo il profilo



$$y_A = \frac{yt}{x_f} \cdot x, \text{ per } 0 < x < x_f; \frac{dy_A}{dx} = \frac{yt}{x_f}$$

$$y_A = \frac{yt}{(c-x_f)} \cdot (c-x), \text{ per } x_f < x < c; \frac{dy_A}{dx} = -\frac{yt}{c-x_f}$$

$$y_b = 0 \text{ in } 0, x_f \text{ e } c$$

$$\int_0^c \left( \frac{dy}{dx} \right)^2 dx = \int_0^{x_f} \left( \frac{yt}{x_f} + \frac{dy_b}{dx} \right)^2 dx + \int_{x_f}^c \left( -\frac{yt}{c-x_f} + \frac{dy_b}{dx} \right)^2 dx =$$

$$= \left[ \frac{yt^2}{x_f} + \int_0^{x_f} \left( \frac{dy_b}{dx} \right)^2 dx + \frac{yt^2}{(c-x_f)} + \int_{x_f}^c \left( \frac{dy_b}{dx} \right)^2 dx \right]$$

ANALOGAMENTE PER LA FACCIA DI SOTTO SOSTITUISCO NEW EC...

$$C_D = \frac{2}{\sqrt{M_{\infty}^2 - 1}} \cdot \left[ \int_0^c \left( \frac{dy_A}{dx} \right)^2 dx + \int_0^c \left( \frac{dy_B}{dx} \right)^2 dx \right]$$

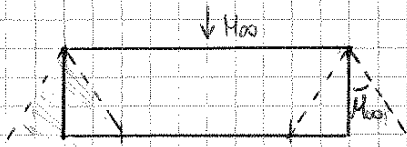
SI VERIFICA CHE IL MINIMO DI  $C_D$  SI HA PER  $\frac{dy_b}{dx} = 0$  VALEA O.R.E PER IL PROFILO A ROTONDO

$$C_{D \text{ MIN}} = \frac{2}{\sqrt{M_{\infty}^2 - 1}} \cdot 4 \left( \frac{yt}{c} \right)^2$$

$$C_{D \text{ MIN}} = \frac{2}{\sqrt{M_{\infty}^2 - 1}} \cdot 4 \left( \frac{t-yt}{c} \right)^2, \text{ per } x_f = \frac{c}{2}; yt = \frac{t}{2}$$

## EFFETTI BIDIMENSIONALI

SUPPONIAMO UNA PACCIA PIANA DI DIMENSIONI FINITE



$$\sin M_{\infty} = \frac{1}{M_{\infty}}$$

$$C_{L_{2D}} = \frac{4\alpha}{\sqrt{M_{\infty}^2 - 1}}$$

$$\text{• PER L'ALA INFINITAMENTE LUNGA, } C_{p_u} = -C_{p_l} = -\frac{2\alpha}{\sqrt{M_{\infty}^2 - 1}}$$

Indico con  $L_{u, g}$  gli effetti reali e con  $L_{2D}$  il caso ideale. NEL CASO REALE HO PERDITE DI PORTANZA.

$$\Delta = L_{2D} \cdot L_w \quad \frac{C_{L_w}}{C_{L_{2D}}} = 1 - \frac{1}{2A\sqrt{M_{\infty}^2 - 1}}$$

$$A = \frac{b}{c} \text{ ALLUNGAMENTO ALARE}$$

A PARITA' DI  $M_{\infty}$ , se  $A \uparrow$ ,  $\frac{C_{L_w}}{C_{L_{2D}}} \rightarrow 1$ , si riduce il peso degli effetti

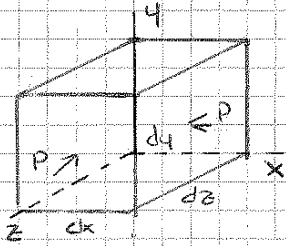
A PARITA' DI  $A$ , se  $M_{\infty} \uparrow$ ,  $\frac{C_{L_w}}{C_{L_{2D}}} \rightarrow 1$ , si restringe il cono di MACH e i suoi effetti sul profilo

• SE IL BORDO D'ATTACCO DELL'ALA E' FUORI DAL CONO DI MACH, ALLORA IL PROFILO E' SUPERSONICO.

# EFFETTI DELLA VISCOSITA' E DELLA CONDUCEBILITA' TERMICA

- VISCOSITA'  $\mu \rightarrow$  GRADIENTI DI VELOCITA' GENERANO SFORZI VISCOSI
- CONDUCEBILITA'  $\lambda \rightarrow$  " " TEMPERATURA " " FLUSSI DI ENERGIA

$\rightarrow$  PUNTO DI VISTA EULERIANO (CONSERVATIVO) = VOLUME DI CONTROLLO FISSO  
 $\rightarrow$  " " " " LAGRANGIANO (NON CONSERVATIVO) = SEGUO LA PARTICELLA FLUIDA.



$$\mu \neq 0 \begin{cases} P_i \\ \tau_{ij} \end{cases}$$

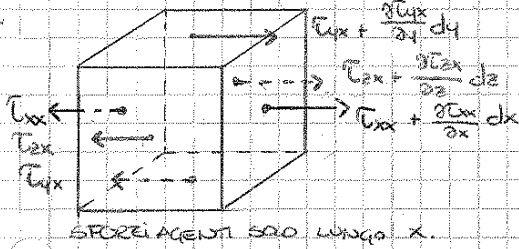
$\rightarrow$  EQ DI CONTINUITA' (NON VARIA)

$$\frac{\partial \rho}{\partial t} + \frac{\partial \rho u}{\partial x} + \frac{\partial \rho v}{\partial y} + \frac{\partial \rho w}{\partial z} = 0$$

FORTE EULERIANA

$$\frac{D\rho}{Dt} = -\rho \nabla \cdot \vec{v}$$

FORTE LAGRANGIANA



$\rightarrow$  BILANCIO DELLA QDM

$$\begin{aligned} & [(P - \tau_{xx})dydz + (\tau_{xx} + \frac{\partial \tau_{xx}}{\partial x} dx - P - \frac{\partial P}{\partial x} dx)dydz] + \\ & + [-\tau_{yx} dx dz + (\tau_{yx} + \frac{\partial \tau_{yx}}{\partial y} dy) dx dz] + \\ & + [-\tau_{zx} dx dy + (\tau_{zx} + \frac{\partial \tau_{zx}}{\partial z} dz) dx dy] = m \cdot a_x \end{aligned}$$

SFORZI AGENTI SULLO SPINGO X.

dove  $m = \rho dx dy dz$  e  $a_x = \frac{Du}{Dt} = \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z}$

Analogamente per y e z, riordino e divido per dx dy dz

$$x) \rho \left( \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) = -\frac{\partial P}{\partial x} + \frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{xy}}{\partial y} + \frac{\partial \tau_{xz}}{\partial z}$$

$$y) \rho \left( \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right) = -\frac{\partial P}{\partial y} + \frac{\partial \tau_{xy}}{\partial x} + \frac{\partial \tau_{yy}}{\partial y} + \frac{\partial \tau_{yz}}{\partial z}$$

$$z) \rho \left( \frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right) = -\frac{\partial P}{\partial z} + \frac{\partial \tau_{xz}}{\partial x} + \frac{\partial \tau_{yz}}{\partial y} + \frac{\partial \tau_{zz}}{\partial z}$$

DIMENSIONALMENTE SI TRATTA DI FORZE PER UNITA' DI VOLUME ( $N/m^3$ )

PER L'EQUILIBRIO ALLA ROTAZIONE SI OTTIENE:

$$\begin{cases} \tau_{xy} = \tau_{yx} \\ \tau_{xz} = \tau_{zx} \\ \tau_{yz} = \tau_{zy} \end{cases} \quad \text{e} \quad \tau_{ij} = \begin{bmatrix} \tau_{xx} & \tau_{xy} & \tau_{xz} \\ \tau_{xy} & \tau_{yy} & \tau_{yz} \\ \tau_{xz} & \tau_{yz} & \tau_{zz} \end{bmatrix} \quad \begin{array}{l} \text{TENSORE DEGLI} \\ \text{SFORZI VISCOSI} \end{array}$$

GLI SFORZI VISCOSI DETERMINANO LE DEFORMAZIONI A VELOCITA' COSTANTE

$$\begin{aligned} \tau_{xx} &= 2\mu \frac{\partial u}{\partial x} + \lambda \nabla \cdot \vec{v} & \tau_{xx} &= \mu \left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial x} \right) = \tau_{yx} & \lambda &= -\frac{2}{3}\mu \\ \tau_{yy} &= 2\mu \frac{\partial v}{\partial y} + \lambda \nabla \cdot \vec{v} & \tau_{xz} &= \mu \left( \frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right) = \tau_{zx} & & \\ \tau_{yz} &= 2\mu \frac{\partial w}{\partial z} + \lambda \nabla \cdot \vec{v} & \tau_{xy} &= \mu \left( \frac{\partial v}{\partial x} + \frac{\partial w}{\partial y} \right) = \tau_{yx} & & \end{aligned}$$

COEFFICIENTE DI STOKES  
O SECONDO COEFF. DI VISCOSITA'

IN FORMA COMPATTA  $\tau_{ij} = \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} - \frac{2}{3} \frac{\partial u_k}{\partial x_k} \delta_{ij} \right)$  con  $\delta_{ij} = \begin{cases} 0 & \text{se } i \neq j \\ 1 & \text{se } i = j \end{cases}$

SOSTITUENDO  $\tau_{ij}$  NELLE EQ LUNGO I 3 ASSI OTTIENGO LE EQUAZIONI DI NAVIER-STOKES (NON-LINEARI, CON SOLUZIONI SOLO IN CASI SEMPLICI).  
 SE IL FLUSSO FOSSE INCOMPRESSIBILE ( $P = \text{cost}$ ), DALLA CONTINUITA' AVREI CHE LA DIVERGENZA E' NULLA.

- PER RISOLVERE LE EQ DI NAVIER-STOKES SI IMPIEGANO SITUAZIONI NUMERICHE DIRETTE.

• IN FORMA COMPATTA:

$$\rho \frac{D(e + v^2/2)}{Dt} = \underbrace{\left[ -\nabla \cdot (p \cdot \vec{v}) \right]}_{\text{PRESSIONE}} + \underbrace{\left[ \vec{T} \cdot \vec{v} \right]}_{\text{VISCOSITÀ}} + \underbrace{\left[ \rho \dot{q} - \frac{\partial q_x}{\partial x} - \frac{\partial q_y}{\partial y} - \frac{\partial q_z}{\partial z} \right]}_{\text{CALORE}}$$

SAPEVAMO CHE  $\rho \frac{D(e + v^2/2)}{Dt} = \rho \frac{D(h + v^2/2)}{Dt} - \frac{\partial p}{\partial t} \cdot \nabla \cdot (\rho \cdot \vec{v})$

E ASSUMENDO:

- FLUSSO STAZIONARIO  $\frac{\partial h}{\partial t} = 0, \frac{\partial p}{\partial t} = 0$
- FLUSSI ESTERNI DI CALORE NULLI ( $q = 0, \rho \dot{q} = 0$ )

OBTENIAMO

$$\rho \cdot \mu_s \frac{\partial h}{\partial x_s} = \frac{\partial p}{\partial t} + \frac{\partial (\tau_{is} \mu_s - q_i)}{\partial x_s} \quad \text{Eq. ENERGIA}$$

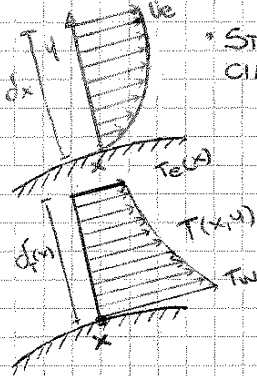
RIASSUMENDO LE EQUAZIONI

• CONTINUITÀ  $\Rightarrow \frac{\partial \rho}{\partial t} + \frac{\partial (\rho u_s)}{\partial x_s} = 0$

• Q.D.M  $\Rightarrow \rho \frac{\partial u_i}{\partial t} + \rho \mu_s \frac{\partial u_i}{\partial x_s} = - \frac{\partial p}{\partial x_i} + \frac{\partial (\tau_{is})}{\partial x_s}$

• ENERGIA  $\Rightarrow \rho \frac{\partial h}{\partial t} + \rho \mu_s \frac{\partial h}{\partial x_s} = \frac{\partial p}{\partial t} + \frac{\partial (\tau_{is} \mu_s - q_i)}{\partial x_s}$

APPLICAZIONE ALLO STRATO LIMITE



• STRATO LIMITE CINEMATICO

$$\tau_{xy} = \mu \left( \frac{\partial u}{\partial y} \right)$$

$$\tau_w = \mu \left( \frac{\partial u}{\partial y} \right)_{y=0} \quad (\text{A PARETE})$$

• STRATO LIMITE TERMICO

$$q_y = -\lambda \left( \frac{\partial T}{\partial y} \right)$$

$$q_w = -\lambda \left( \frac{\partial T}{\partial y} \right)_{y=0} \quad (\text{A PARETE})$$

$$Re = \frac{V_{\infty} L \rho_{\infty}}{\mu}$$

$$Pr = \frac{\mu \cdot c_p}{\lambda}$$

Per uno strato limite laminare, si ha che:  $Pr \cdot d \sqrt{\frac{\delta(x)}{\delta(x)}}$

OSSIA IL PRANDTL E' PROPORZIONALE AL RAPPORTO DELLE ESTENSIONI DEGLI STRATI LIMITE.

$$Pr = \frac{48}{98.5} \quad (\text{ARIA } Pr = 0,71)$$

EQ. DELLO STRATO LIMITE 2D, STAZIONARIO, COMPRESSIBILE e TERMICO

2D implica  $w=0, \frac{\partial}{\partial z}=0$   
LE EQUAZIONI DIVENTANO:

• CONTINUITÀ:  $\frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} = 0$

• Q.D.M 
$$\begin{cases} \rho \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = - \frac{\partial p}{\partial x} + \frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{yx}}{\partial y} \\ \rho \left( u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = - \frac{\partial p}{\partial y} + \frac{\partial \tau_{xy}}{\partial x} + \frac{\partial \tau_{yy}}{\partial y} \end{cases}$$

• ENERGIA:  $\rho \left[ u \frac{\partial h}{\partial x} + v \frac{\partial h}{\partial y} \right] = \frac{\partial (\tau_{xx} u + \tau_{xy} v - q_x)}{\partial x} + \frac{\partial (\tau_{yx} u + \tau_{yy} v - q_y)}{\partial y}$

ASSUNZIONI:

$Re \gg 1, \quad \delta/L \ll 1, \quad \tau_{yx} = \mu \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)$  TRASCURABILE,  $T = \frac{h}{c_p}$

• dalla CONTINUITÀ  $\rightarrow \rho \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = - \frac{dp}{dx} + \frac{\partial \tau_{yx}}{\partial y}$   
 $\rightarrow \frac{\partial p}{\partial y} = 0$  LO STRATO LIMITE E' SOLO LUNGO Y

• dall' ENERGIA  $\rightarrow \rho \left[ u \frac{\partial h}{\partial x} + v \frac{\partial h}{\partial y} \right] = \frac{\partial}{\partial y} \left[ \mu \frac{\partial u^2/2}{\partial y} + \frac{\lambda}{c_p} \frac{\partial h}{\partial y} \right] = \frac{\partial}{\partial y} \left[ \mu \left( \frac{\partial u^2/2}{\partial y} + \frac{\lambda}{c_p} \frac{\partial h}{\partial y} \right) \right]$

con  $q_w \neq 0, dp/dx \neq 0, Pr \neq 1$  NON ESISTONO SOLUZIONI E DEVO STUDIARE FLUSSI SIMILI.

**PROFILO DI TEMPERATURA: CASO ADIABATICO (Pr ≠ 1)**

$\frac{dPe}{dx} = 0, Pr \neq 1, q_w = 0$

$H = H_e = H_w = \text{cost.}$

$h_{00} + \frac{U_{00}^2}{2} = h_e + \frac{u_e^2}{2}$



GIÀ IL PUNTO DI ARRESTO ISOENTROPICO

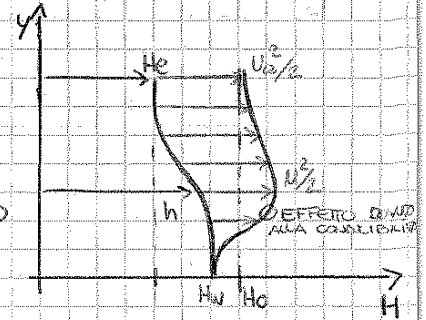
$H_{00} = H_0$   
 $T_w = T_0$   
 $U = 0$

Se  $Pr \neq 1, h + R \frac{u^2}{2} = \text{cost.}$

$H_r = h_e + R \frac{u_e^2}{2} = H_w$  entalpia di recupero

$T_r = T_e + R \frac{u_e^2}{2c_p} = T_e (1 + \frac{\gamma-1}{2} M_e^2)$

- $R = Pr^{1/2}$  LAMINARE
- $R = Pr^{1/3}$  TURBOLENTO
- $R = Pr$  COELETTE



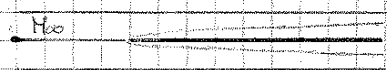
PROFILO DI TEMPERATURA  $T = T_e + R \frac{u_e^2}{2c_p} (1 - \varphi^2)$

**PROFILO DI TEMPERATURA: CASO NON ADIABATICO**

$q_w = 0, Pr \neq 1, \frac{dPe}{dx} \neq 0, (-\lambda \left(\frac{\partial T}{\partial y}\right)_{y=0})$  NON HO SOLUZIONI.

• SEMPLIFICAZIONE:  $Pr = 1, \frac{dPe}{dx} = 0, \frac{\partial^2}{\partial x^2} = 0$

PIACCA PIANA A INCIDENZA NULLA



**INTEGRALE DI CROCCO**

$H = C_1 + C_2 u$   $M \rightarrow Q.D.H, H \rightarrow \text{ENERGIA}$

per trovare  $C_1$  e  $C_2$  impongo le condizioni iniziali e al contorno

$y=0, u_w=0 \rightarrow$  Aderenza A PARETE  
 $H_w = C_p T_w \rightarrow$  Eq termico

$y=\infty, u = u_e \rightarrow$  Aderenza ESTERNO  
 $H_e = H_{00} \rightarrow$  Eq

$\rightarrow y=0, u=0, H=H_w \rightarrow C_1 = H_w$   
 $y=\infty, u=u_e, H=H_e \rightarrow C_2 = (H_e - H_w) \cdot \frac{1}{u_e}$

Per tanto  $H = H_w + \frac{H_e - H_w}{u_e} \cdot u$

$\frac{u}{u_e} = \frac{H - H_w}{H_e - H_w} = \frac{h + \frac{u^2}{2} - h_w}{h_e + \frac{u_e^2}{2} - h_w}$  ANALOGIA TRA CARICO DI VELOCITA' ED ENERGIA

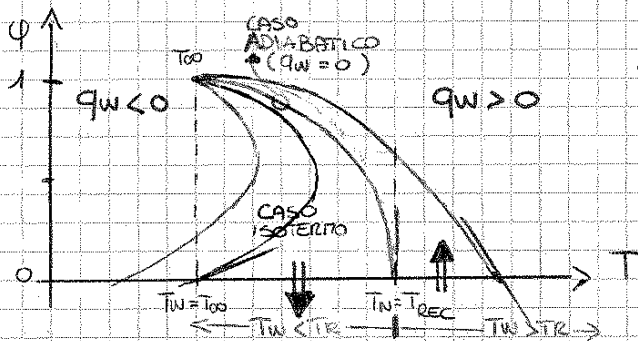
• PROFILI DI TEMPERATURA;  $T = T(\varphi)$  e  $\varphi = u/u_e$

$T (1 + \frac{\gamma-1}{2} M^2) = \varphi [T_{00} (1 + \frac{\gamma-1}{2} M_{00}^2) - T_w] + T_w$

$T = T_w (1 - \varphi) + T_{00} \varphi^2 + T_0 (\varphi - \varphi^2)$ , con  $T_0 = T_w (1 + \frac{\gamma-1}{2} M_{00}^2)$  se  $Pr = 1$

se  $q_w \neq 0, Pr \neq 1$  e  $\frac{dPe}{dx} \neq 0$ , correggo il profilo con R

$T = T_w (1 - \varphi) + T_{00} \varphi^2 + T_{rec} (\varphi - \varphi^2)$



- CASEO ADIABATICO ( $T_w = T_r$ )
- CASEO ISOTERMO ( $T_w = T_{00}$ )

- PER  $T_w < T_r$  la parete può essere più calda della corrente ( $T_w > T_{00}$ ), TANTAVIA PER EFFETTO DELL'ATTRITO IL FLUSSO DI CALORE E' DIRETTO DALLA CORRENTE ALLA PARETE

- PER  $T_w > T_r$  LA PARETE E' SUFFICIENTEMENTE CALDA DA TRASMETTERE CALORE AL FLUSSO

Se  $Pr = 1, T_w = T_0$   
Se  $Pr \neq 1, T_w = T_{rec}$

### METODO DELLA SEZIONE RAPPRESENTATIVA

siano  $u(T)$  e  $P(T)$ , scelto  $\phi = 0,5$

•  $T = T_w (1 - \phi) + T_{oo} \phi^2 + T_{rec} (\phi - \phi^2)$   
 $T^* = 0,5 T_w + 0,25 T_{oo} + 0,25 T_{rec}$

$C_{D,COMP} (Re, M_{oo}, T_w/T_{oo}) = C_{D,INCOMP} \cdot X (M_{oo}, \frac{T_w}{T_{oo}})$  dove  $X$  E' UN FATTORE CORRETTIVO.

$Re_{oo} = \frac{V_{oo} L P_{oo}}{\mu_{oo}}$  ;  $\left\{ \begin{array}{l} \text{se } Re_1 < Re_{CR} = 5 \cdot 10^5 \text{ (RACCA FINA)} \rightarrow \text{LAMINARE} \\ \text{se } Re > Re_{CR} \rightarrow \text{TURBOLENTO} \end{array} \right.$

• LAMINARE,  $C_D = \frac{1,328}{\sqrt{Re_{oo}}}$  ;  $Re < 5 \cdot 10^5$

• TURBOLENTO (BASSO),  $C_D = \frac{0,074}{Re_{oo}^{1/2}}$  ;  $5 \cdot 10^5 < Re < 10^7$

• TURBOLENTO (ALTO),  $C_D = \frac{0,0295}{Re_{oo}^{1/2}}$  ;  $Re > 10^7$

$T_w = \frac{1}{2} P_{oo} V_{oo}^2 \cdot C_D$

$X = \frac{C_{D,C}}{C_{D,E}} = \frac{T_w,C}{T_w,E}$

$T_{w,INCOMP} \propto (P_{oo} \mu_{oo})^{1/2}$

$T_{w,COMP} \propto (P_{oo} \mu_{oo})^{1/2}$

$T_{w,COMP} \propto (P_{oo}^* \mu_{oo}^*)^{1/2}$  E' DATA SEZIONE RAPPRESENTATIVA;  $X = \left( \frac{P_{oo}^* \mu_{oo}^*}{P_{oo} \mu_{oo}} \right)^{1/2}$

POICHE'  $\frac{\mu^*}{\mu_{oo}} = \left( \frac{T^*}{T_{oo}} \right)^{\omega}$  e  $\frac{P^*}{P_{oo}} = \left( \frac{T^*}{T_{oo}} \right)^{-2}$  con  $\omega = \omega(T)$ , per  $T \sim 300K$ ,  $\omega = 0,75$

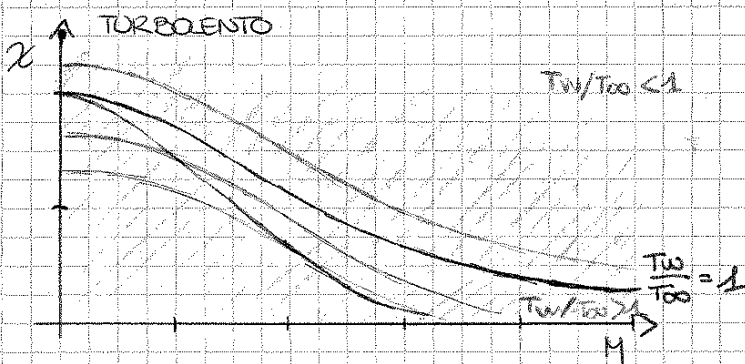
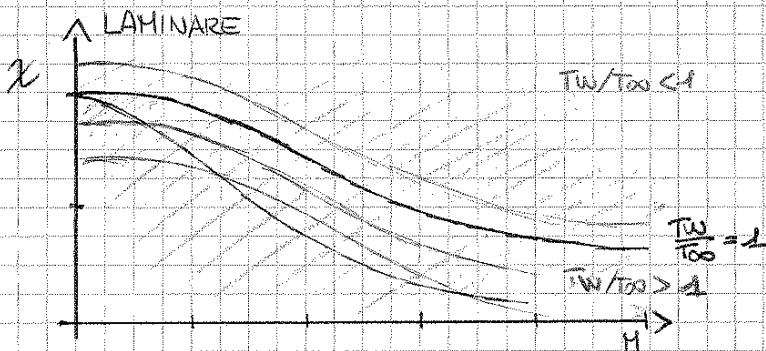
quindi  $X_{LAMI} = \left( \frac{T^*}{T_{oo}} \right)^{\frac{\omega-1}{2}} = \left[ \frac{T_w + T_{oo}}{2 T_{oo}} + R \cdot \frac{\gamma-1}{2} \cdot M_{oo}^2 \cdot \frac{1}{4} \right]^{\frac{\omega-1}{2}}$

$\frac{\omega-1}{2} = 0,125$  ( $T \sim 300K$ )

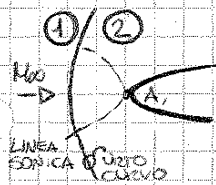
per il turbolento cambiano solo gli esponenti:

$X_{TURB} = \left[ \frac{T_w + T_{oo}}{2 T_{oo}} + R \cdot \frac{\gamma-1}{2} \cdot M_{oo}^2 \cdot \frac{1}{4} \right]^{\frac{\omega-4}{5}}$

$\frac{\omega-4}{5} = -0,65$  ( $T \sim 300K$ )



## FLUSSO DI CALORE NEL PUNTO DI ARRESTO

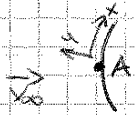


$$P_A = P_2^0 \quad M_A = 0$$

$$T_A = T_2^0 = T_2^* = T_2^{\infty} \quad T_2^*/T_2^* = f(M)$$

Se  $M_{\infty} > 1$ , l'urto è curvo; in A,  $\begin{cases} T_w = 0 \\ q_w = \max \end{cases}$   
 ( $3 < M_{\infty} < 10$ )

### FLUSSO NELL'INTORNO DEL PUNTO DI ARRESTO INCOMPRESSIBILE



$$U_e(x) = K \cdot x \quad U_e(A) = 0 \quad (x_A = 0) \quad \left( \frac{dU_e}{dx} \right)_{x=0} = K \quad \text{PUE} \quad \frac{dU_e}{dx} = \frac{dP_e}{dx} \quad \text{GRADIENTE DI PRESSIONE}$$

### METODI DI RISOLUZIONE INTEGRALI

• Si perdono soluzioni locali a beneficio di una soluzione GLOBALE

$$\delta^* = \text{SPESORE DI SPOSTAMENTO} \quad \theta = \text{SPESORE DI QUANTITÀ DI MOTO} \quad x \rightarrow \begin{cases} \delta^*(x) \\ \theta(x) \\ CF(x) \rightarrow T_w(x) \end{cases}$$

$$H = \frac{\delta^*}{\theta} = \text{PARAMETRO DI FORTE} \quad \delta^* = \int_0^{\infty} \left(1 - \frac{U}{U_e}\right) dy \quad \theta = \int_0^{\infty} \frac{U}{U_e} \left(1 - \frac{U}{U_e}\right) dy$$

$H = 2,5 \rightarrow$  STRATO LIMITE LAMINARE  
 $H = 1,3 \rightarrow$  STRATO LIMITE TURBOLENTO

### METODO DI THWAITES (X IL FLUSSO LAMINARE)

NOTO IL FLUSSO ESISTENTE FORNISCE FACILMENTE  $\theta^2(x) = \frac{0,45 \nu}{U_e(x)^3} \int_0^x U_e(x) dx$

NELL'INTORNO DEL PUNTO DI ARRESTO (dove  $K = \left(\frac{dU_e}{dx}\right)_{x=0}$ )

$$\theta^2(x)_{\text{ARRESTO}} = \frac{0,45 \nu}{K^3 x^6} \int_0^x (Kx)^5 dx = \frac{0,45 \nu}{6K} \quad \text{OSSIA È GIÀ PRESENTE LO STRATO LIMITE E } \theta \text{ È COSTANTE}$$

CONSIDERIAMO:  $\lambda = \frac{\theta^2}{\nu} \left(\frac{dU_e}{dx}\right)$  e  $P = \left(\frac{dU}{dy}\right)_{y=0} \cdot \frac{\theta}{U_e(x)} = P(\lambda)$

PER FLUSSI ACCELERATI:  $P = 0,22 + 1,67\lambda - 1,8\lambda^2 \quad (\lambda > 0)$

PER IL PT. DI ARRESTO:  $\lambda_{\text{ARR}} = \theta_{\text{ARR}} + \frac{\nu}{U_e} = 0,075$

$$P_{\text{ARR}} = P(\lambda_{\text{ARR}}) = 0,328$$

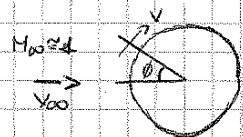
da cui, sostituendo:  $T_w = 0,328 \cdot \frac{x}{R} = f(x, U, P, K)$  e  $K = P \left( \frac{\text{FORZA GEOMETRICA}}{V_{\infty}} \right)$

### APPLICAZIONE (SFERA - CILINDRO)

$V(\phi) = 2V_{\infty} \sin \phi$ , con  $\phi = \frac{y}{R} \rightarrow$  FLUSSO POTENZIALE

$V(x) = 2V_{\infty} \sin\left(\frac{y}{R}\right) \rightarrow$  Approssimazione  $U_e(x) = V(x)$

$\frac{dV}{dx} = 2V_{\infty} \cos\left(\frac{y}{R}\right) = K \Big|_{x=0} \Rightarrow$  SFERA =  $4V_{\infty}/D \rightarrow K = \frac{4D}{V_{\infty}}$   
 CILINDRO =  $3V_{\infty}/D \rightarrow K = \frac{3D}{V_{\infty}}$



per flussi ipersonici incompressibili:

CILINDRO:  $T_w(x) = 1,232 \cdot \sqrt{P_{\infty} M_{\infty} U_{\infty}^2} \left(\frac{dU_e}{dx}\right)$   
 $q_w(x) = 0,57 Pr^{-0,6} (Pe We K)^{1/2} \left(\frac{P_{\infty} U_{\infty}}{Pe We}\right)^{0,1} (T_e - T_w)$

$w =$  parete  
 $e =$  esterno

SFERA:  $T_w(x) = 1,312 \cdot \sqrt{P_{\infty} M_{\infty} U_{\infty}^2} \left(\frac{dU_e}{dx}\right)$   
 $q_w(x) = 0,763 Pr^{-0,6} (Pe We K)^{1/2} \left(\frac{P_{\infty} U_{\infty}}{Pe We}\right)^{0,1} (T_e - T_w)$

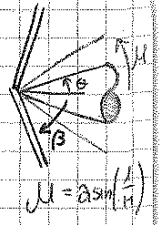


# FORMULARIO

## • URTI

$$\begin{aligned} P_1 &< P_2 & T_{01} &= T_{02} \\ T_1 &< T_2 & V_1 &> V_2 \\ P_{01} &< P_{02} & P_{01} &> P_{02} \\ S_1 &< S_2 & M_{01} &> M_{02} \end{aligned}$$

$$\begin{aligned} T^0 &= T \cdot \left(1 + \frac{\gamma-1}{2} M^2\right) \\ P^0 &= P \cdot \left(1 + \frac{\gamma-1}{2} M^2\right)^{\frac{\gamma}{\gamma-1}} \\ P^{00} &= P \cdot \left(1 + \frac{\gamma-1}{2} M^2\right)^{\frac{1}{\gamma-1}} \\ a &= \sqrt{\gamma R T} = \sqrt{\gamma P/\rho} \end{aligned}$$



## • RETTO

$$V_1 \cdot V_2 = V_{cr}^2 = a^{*2}$$

$$1 < M_2 < 0,45 \quad (\gamma=1,4, M_2 \leq 5)$$

$$M_2^2 = \frac{2 + (\gamma-1)M_1^2}{2\gamma M_1^2 - (\gamma-1)} \quad ; \quad M_1^2 = \frac{2 + (\gamma-1)M_2^2}{2\gamma M_2^2 - (\gamma-1)}$$

$$\frac{P_2}{P_1} = 1 - \frac{2\gamma}{\gamma-1} \cdot (M_1^2 - 1) \quad ; \quad \frac{P_2}{P_1} = \frac{V_1}{V_2} = \frac{(\gamma+1)M_1^2}{2 + (\gamma-1)M_1^2} \quad ; \quad \frac{T_2}{T_1} = 1 + \frac{2(\gamma-1)}{(\gamma+1)^2} \cdot \frac{\gamma M_1^2 + 1}{M_1^2} \cdot (M_1^2 - 1)$$

$$\frac{P_{02}}{P_{01}} = \frac{P_2}{P_1} \cdot \left[1 + \frac{2\gamma}{\gamma+1} \cdot (M_1^2 - 1)\right]^{-\frac{1}{\gamma-1}} \cdot \left[\frac{(\gamma+1)M_1^2}{2 + (\gamma-1)M_1^2}\right]^{\frac{\gamma}{\gamma-1}}$$

$$\frac{S_2 - S_1}{R^*} = -\ln \frac{P_{02}}{P_{01}} = \frac{\gamma}{\gamma-1} \cdot \ln \frac{T_2}{T_1} = \ln \frac{P_2}{P_1}$$

$$R^* = c_p - c_v = 287 \text{ J/kg}\cdot\text{K}$$

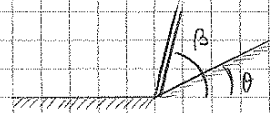
$$c_p = 1005 \text{ J/kg}\cdot\text{K}$$

$$\frac{a^2}{\gamma-1} + \frac{V^2}{2} = \text{const} = \frac{a_0^2}{\gamma-1} = \frac{a^{*2}}{2} \cdot \left(\frac{\gamma+1}{\gamma-1}\right) \quad ; \quad c_p T^0 = c_p T_1 + \frac{V^2}{2}$$

$$M_1^2 = \left(\frac{V}{a^*}\right)^2 = \frac{M^2 (\gamma+1)}{2 + M^2 (\gamma-1)} \rightarrow M^2 = \frac{2}{(\gamma+1)/M^2 - (\gamma-1)} \quad ; \quad S_2 - S_1 = c_v \ln \left[ \frac{1 + \frac{2\gamma}{\gamma-1} (M_1^2 - 1)}{(\gamma-1)} \cdot \frac{2 + (\gamma-1)M_1^2}{(\gamma+1)M_1^2} \right]^{\frac{\gamma}{\gamma-1}}$$

## • OBLIQUO

$$V_{N1} \cdot V_{N2} = V_{cr}^2 = \frac{(\gamma-1)}{(\gamma+1)} V^2$$

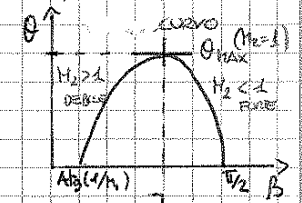


$$\frac{1}{\tan(\theta)} = \left(\frac{\gamma+1}{2} \cdot \frac{M^2 \sin^2(\beta)}{M^2 \sin^2(\beta) - 1}\right) \cdot \tan(\beta)$$

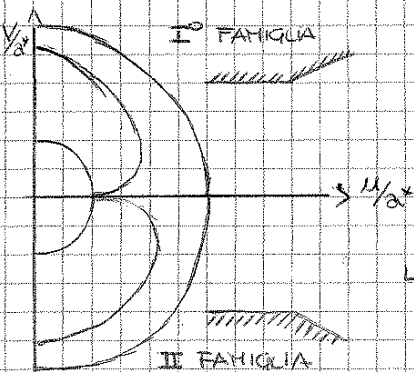
\* Valgono, con  $M_1 \rightarrow M_{1N} = M_1 \cdot \sin(\beta)$

$$F_1 \cdot [M_2 \cdot \sin(\beta - \theta)]^2 = \frac{2 + (\gamma-1)(M_1 \cdot \sin \beta)^2}{2\gamma (M_1 \cdot \sin \beta)^2 - (\gamma-1)}$$

$$\tan(\theta) = \frac{2}{\tan(\beta)} \cdot \frac{M^2 \sin^2 \beta - 1}{M^2 (\gamma + \cos(2\beta)) + 2}$$



## • ESPANSIONI



DATI  $M_1, \theta_w$

$$\nu(M_1) = \left[ \sqrt{\frac{\gamma+1}{\gamma-1}} \cdot \arctg\left(\sqrt{\frac{\gamma-1}{\gamma+1}} \sqrt{M_1^2 - 1}\right) + \arctg \sqrt{M_1^2 - 1} \right] \cdot \text{const}$$

$$\left. \begin{aligned} \theta_0 = \nu(M_1) \\ \theta_w = \nu(M_2) \end{aligned} \right\} \begin{aligned} \text{I° FAN} &\rightarrow \theta_w - \nu(M_1) = \text{const} = \theta_w - \theta_0 \\ \text{II° FAN} &\rightarrow \theta_w + \nu(M_1) = \text{const} = \theta_w + \theta_0 \end{aligned}$$

$$\theta_0 + \theta_w = \theta_2 = \nu(M_2) \Rightarrow M_2 \text{ (iterativo)}$$

L'ESP E' ISENTROPICA

$$\begin{cases} T_1^0 = T_2^0 \\ P_1^0 = P_2^0 \\ \rho_1^0 = \rho_2^0 \end{cases}$$

• STRATO LIMITE TERMICO

ARIA STANDARD

FOURIER:  $q = -\lambda \text{ grad } T \rightarrow q_y = -\lambda \frac{\partial T}{\partial y}$

PRANDTL:  $Pr = \frac{\mu c_p}{\lambda} = \frac{\nu}{\alpha} = \frac{48}{98-5} = \frac{2L+4}{2L+9}$ ;  $Pr \propto \left(\frac{\delta}{\delta_T}\right)^2$

$\mu = 1,781 \cdot 10^{-5} \text{ Kg/m}\cdot\text{s}$   
 $\nu = 1,654 \cdot 10^{-5} \text{ m}^2/\text{s}$   
 $T = 288 \text{ K}$   
 $c_p = 1005$   
 $R = 287$   
 $\gamma = 1,4$   
 $\rho = 1,225 \text{ Kg/m}^3$

• CASO ADIABATICO ( $q_w = 0$ )  
 $Pr = 1$

BOSEMANN:  $H = h + \frac{u^2}{2} = h_{\infty} + \frac{u_{\infty}^2}{2} = h_e + \frac{u_e^2}{2} = h_w = H^0 = \text{COSTANTE}$   
 $T = T_e + \frac{u_e^2}{2c_p} (1 - \varphi^2)$  con  $\varphi = \frac{u}{u_e}$   
 $T_w (\varphi=0) = T_e + \frac{u_e^2}{2c_p} = T_e \left(1 + \frac{\gamma-1}{2} Ma_e^2\right)$

$Pr \neq 1$

$H_{rec} = h + R \cdot \frac{u^2}{2} = h_e + R \frac{u_e^2}{2} = h_w = \text{COST}$

FATTORE DI RECUPERO  $R \rightarrow$   $\begin{cases} Pr' \rightarrow \text{COSTE} \\ Pr'^{1/2} \rightarrow \text{LAMINARE} \\ Pr'^{1/3} \rightarrow \text{TURBOLento} \end{cases}$

$T = T_e + R \cdot \frac{u_e^2}{2c_p} (1 - \varphi^2)$

$T_w = T_{rec} = T_e + \frac{u_e^2}{2c_p} = T_e \left(1 + \frac{\gamma-1}{2} R Ma_e^2\right)$

• CASO NON ADIABATICO ( $q_w \neq 0$ )

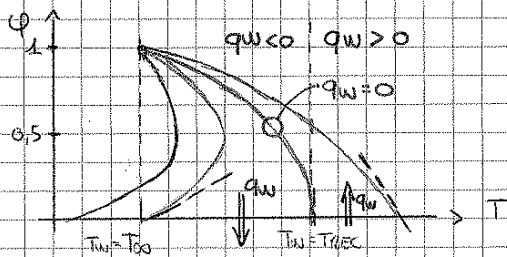
CROCCO  $\Rightarrow H = C_1 + C_2 u$   $\begin{cases} C_1 = H_w \\ C_2 = (H_e - H_w)/u_e \end{cases}$

$H = H_w + \frac{H_e - H_w}{u_e} \cdot u$

$T = T_w (1 - \varphi) + T_{\infty} \varphi^2 + T_0 (\varphi \cdot \varphi^2)$   
 $T = T_w (1 - \varphi) + T_{\infty} \varphi^2 + T_{rec} (\varphi \cdot \varphi^2)$

per  $Pr = 1$   
 per  $Pr \neq 1$

$T_0 = T_w \left(1 + \frac{\gamma-1}{2} Ma_w^2\right)$



$T_{\infty} < T_w < T_0 \rightarrow T_w$  cambiano  $q_w \downarrow$  (seppure  $T_w > T_{\infty}$ )  
 $T_w > T_0 \rightarrow q_w \uparrow$   
 $T_w < T_{\infty} \rightarrow q_w \downarrow$

ANALOGIA DEI CAMPI  $\rightarrow \frac{u}{u_e} = \frac{H - H_p}{H_e - H_p} = \frac{h + \frac{1}{2} u^2 - h_p}{h_e + \frac{1}{2} u_e^2 - h_p}$  (Solo se  $Pr = 1$ )

$T = T_{\infty} \varphi^2 + T_{rec} (1 - \varphi^2)$  CASO ADIABATICO ( $T_w = T_{rec}$ )  
 $T = T_{\infty} + (T_{rec} - T_{\infty})(\varphi - \varphi^2)$  " ISOBARICO ( $T_w = T_{\infty}$ )

ANALOGIA DI REYNOLDS  $\rightarrow \frac{T_w(x)}{u_e} = \frac{-q_w(x)}{h_{\infty} + \frac{1}{2} u_e^2 - h_w}$

$\begin{cases} \alpha = 1, r = 1 & \text{COSTE} \\ \alpha = 1/3, r = 1/2 & \text{LAMINARE} \\ \alpha = 0,6, r = 1/3 & \text{TURBOLento} \end{cases}$

$\frac{T_w(x)}{u_e} = \frac{-A q_w(x)}{c_p (T_{rec} - T_w)} = \frac{-A q_w(x)}{h_{\infty} + R \cdot \frac{1}{2} u_e^2 - h_w}$  se  $Pr \neq 1$

ANALOGIA DEGLI SCAMBI INTEGRALI  $\rightarrow \frac{T_w}{u_e} = \frac{-A \bar{q}_w}{c_p (T_{rec} - T_w)}$

conv. FORZATA  $\bar{q}_w = -RAT = -\frac{T_w}{\sqrt{A}} \cdot c_p (T_{rec} - T_w)$ , con  $R = \rho u_e c_p Ma_e / 2A$

• SEZIONE RAPPRESENTATIVA ( $\varphi = 0,5 \rightarrow T^*, Re^*$ )

$Re = \frac{u_e L \rho u_e}{\mu} \left( \begin{matrix} \text{LAMINARE} \\ 5 \cdot 10^5 \\ \text{P.P.} \end{matrix} \right)$

$T^* = 0,5 T_w + 0,25 T_{\infty} + 0,25 T_{rec}$

$\chi = \text{FATTORE CORRETTIVO}$ :  $\chi_L = \left(\frac{T_w + T_{\infty}}{2 T_{\infty}} + R \frac{\gamma-1}{2} \frac{Ma_e^2}{4}\right)^{-0,125}$   
 $\chi_T = \left(\frac{T_w + T_{\infty}}{2 T_{\infty}} + R \frac{\gamma-1}{2} \frac{Ma_e^2}{4}\right)^{-0,65}$

dove  $c_{f,comp} = c_{f,incorp} \cdot \chi$ ,  $T_{w,c} = \chi \cdot T_{w,inc}$

$C_{D,comp} = C_{D,incorp} \cdot \chi$ ,  $\bar{T}_{w,c} = \chi \bar{T}_{w,inc}$

• FLUSSO DI CALORE SU P.P.

FORMULA DI ROMIG:  $q_w = 0,067 \cdot \rho u_e \sqrt{\frac{\rho u_e}{Re}} \left[ \frac{W}{m^2} \right]$

• MISCELE DI GAS

$X_i = N_i / N_T$  ;  $C_i = m_i / m_T$  ;  $M_T = m_T / N_T = \sum X_i M_i = 1 / \sum C_i / M_i$

DALTON:  $P_T = \sum P_i$  ,  $P_i / P_T = N_i / N_T = V_i / V_T$

SUTHERLAND:  $\mu = S \frac{T^{3/2}}{X+T}$  ,  $X = T_{REF}$  ,  $S = \mu_{T=X}$

WILKE:  $\mu_{MISC} = \sum_i \mu_i \cdot \left( 1 + \sum_k C_{ik} \cdot \frac{X_k}{X_i} \right)^{-1}$   
 $\left[ 1 + \left( \sum_k \left( \frac{\mu_i}{\mu_k} \right)^{1/2} \left( \frac{M_i}{M_k} \right)^{1/4} \right)^2 \right]^{-2}$

dove  $C_{ik} = \frac{2^{3/2} \cdot [1 + (M_i / M_k)]^{1/2}}$

$C_V = 2 \cdot \frac{R}{M} = \frac{\gamma}{\gamma-1} \cdot \frac{R}{M}$

$C_P = \frac{\gamma+2}{2} \cdot \frac{R}{M} = \frac{1}{\gamma-1} \cdot \frac{R}{M}$

$\gamma = \frac{\gamma+2}{2} = \frac{C_P}{C_V}$  ;  $R = C_P - C_V$

$\frac{P_2}{P_1} = \left( \frac{T_2}{T_1} \right)^{\frac{\gamma}{\gamma-1}}$  ,  $\frac{P_2}{P_1} = \left( \frac{T_2}{T_1} \right)^{\frac{1}{\gamma-1}}$   
 $\frac{P_2}{P_1} = \left( \frac{P_2}{P_1} \right)^\gamma$  ,  $\left( \frac{P}{P} \right)^\gamma = \text{cost}$

EQ. ENTROPIA:  $S_2 - S_1 = C_P \cdot \ln(T_2/T_1) - R^* \cdot \ln(P_2/P_1)$   
 $S_2 - S_1 = C_V \cdot \ln(T_2/T_1) + R^* \cdot \ln(P_1/P_2)$

• FORZE E MOMENTI

$C_P = \frac{P - P_{00}}{1/2 \rho_{00} V_{00}^2}$  ;  $C_D = \frac{D}{1/2 \rho_{00} V_{00}^2 S}$  ;  $C_M = \frac{M}{1/2 \rho_{00} V_{00}^2 S L}$

• CROCCO

$T \nabla \Delta = \nabla H - \nabla \times \nabla \times \nabla + \frac{\partial \nabla}{\partial t}$   
ENTROPIA      ENTAPIA      VELOCITÀ

• VEL. POTENZIALE

$\nabla = \nabla \phi \rightarrow u_i + v_j + w_k = \frac{\partial \phi}{\partial x} i + \frac{\partial \phi}{\partial y} j + \frac{\partial \phi}{\partial z} k$

• MECCANICA STATISTICA

$V_{AT} = \sqrt{2E_g/m}$  ;  $V_{AT} = \sqrt{\frac{3RT}{M}}$   
 $E_g = \frac{3}{2} K_b T$

$K_b = 1,38 \cdot 10^{-6}$

KNUDSEN  $K_N = \frac{P}{L}$  ,  $P = \frac{1}{d^2} n \cdot \frac{1}{\sqrt{2}} \pi$

$E = \frac{L}{2} RT$  (con moltiplicazione) ;  $M = \frac{L+2}{2} RT$

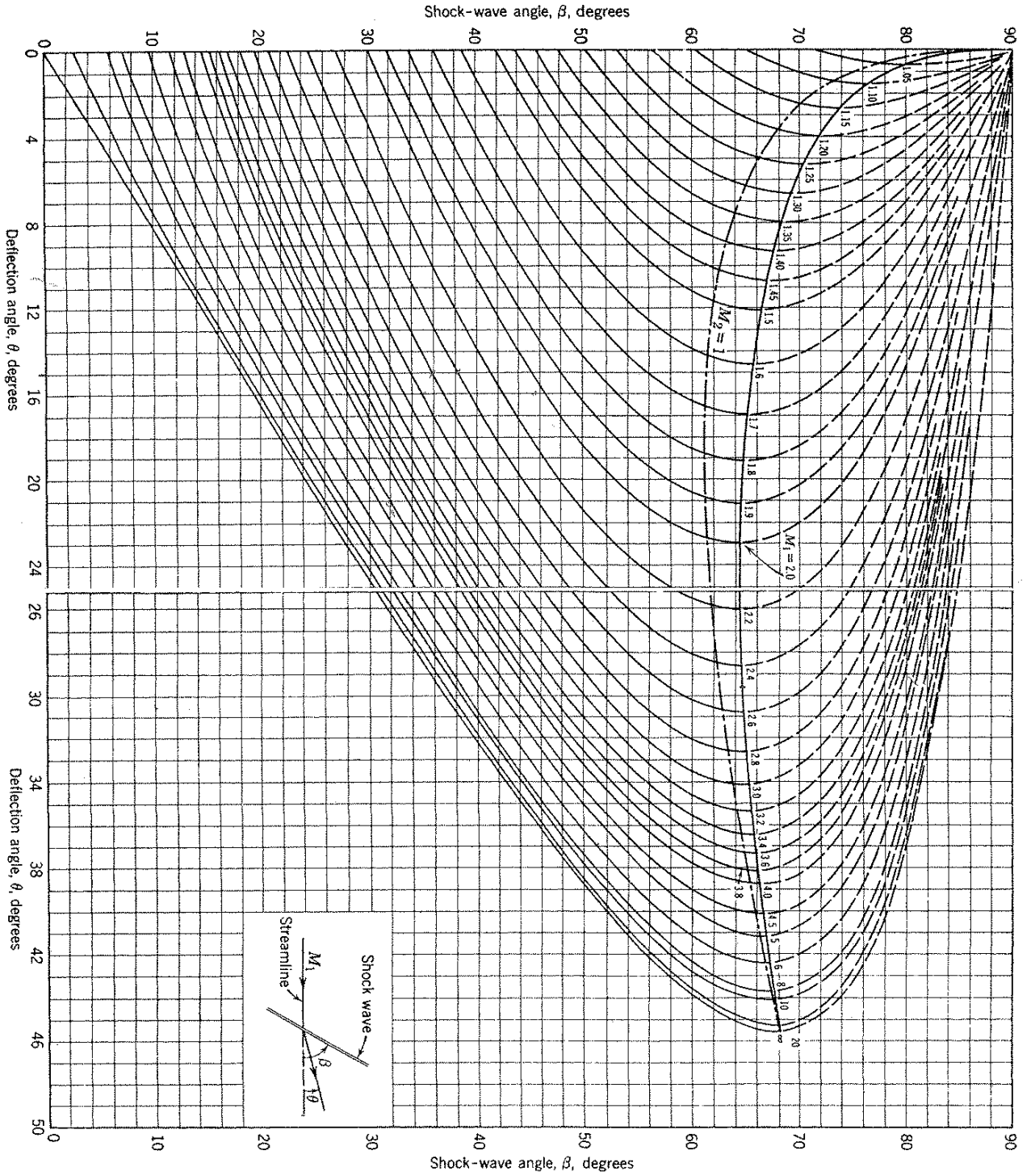
• EQUAZIONI FLUSSI 1D

• C  $Pu = \text{cost}$

• QOT  $P + \rho u^2 = \text{cost}$

• E  $H_1 + q = H_2$

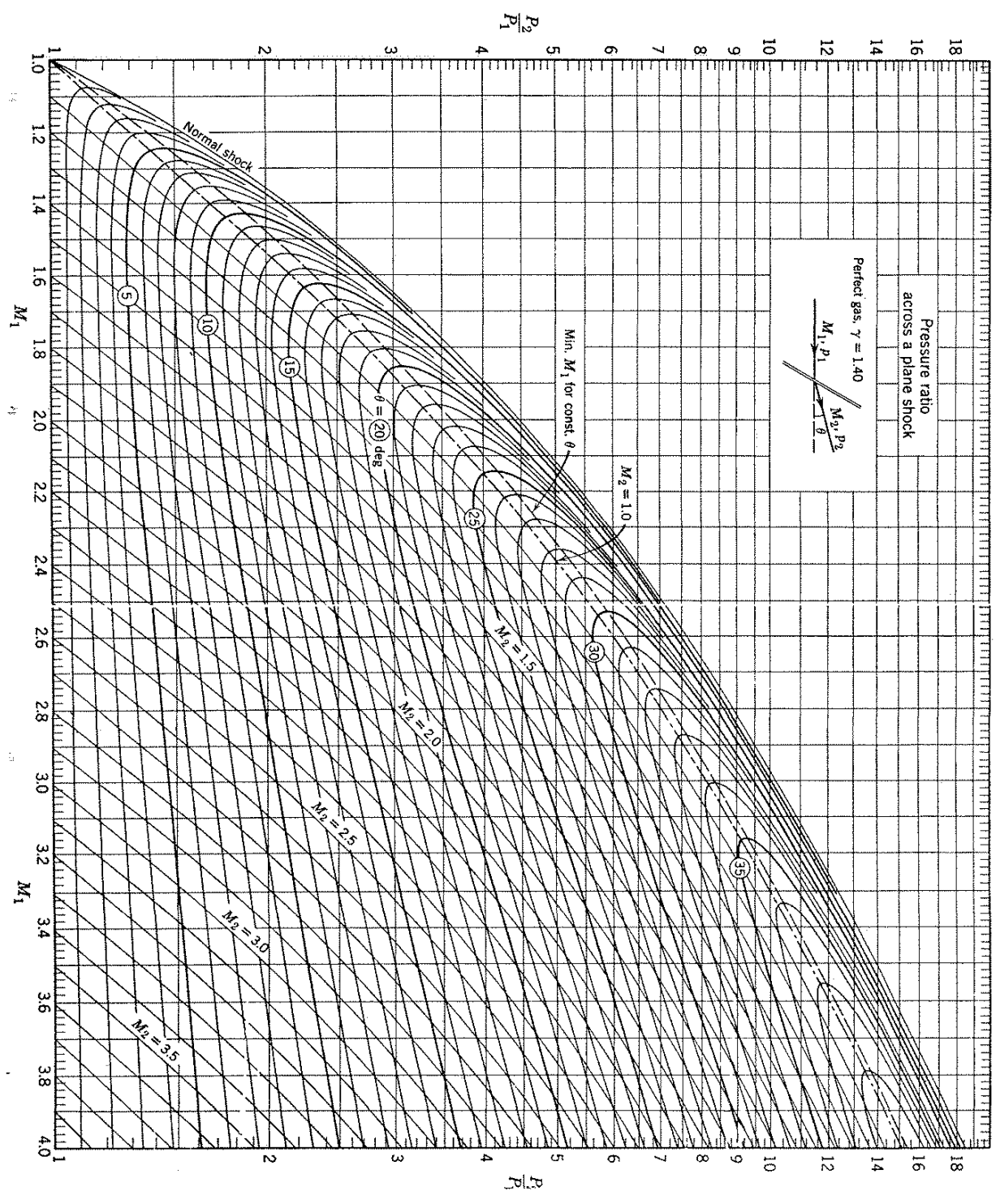




Oblique Shock Chart 1 Variation of shock-wave angle with flow-deflection angle for various upstream Mach numbers. Perfect gas,  $\gamma = 1.40$ . (From NACA Report 1135.)

Chart 1 (continued)

376  
830



OBlique SHOCK CHART 2 Variation of pressure ratio and downstream Mach number with flow-deflection angle and upstream Mach number. (Data from C. L. Dailey and F. C. Wood, *Computation Curves for Compressible Flow Problems*, Wiley, 1949.)

CHART 2 (continued)

TABLES

TABLE II

Flow Parameters Versus M for Subsonic Flow

M	$p/p_0$	$\rho/\rho_0$	$T/T_0$	$a/a_0$	$A^*/A$
.00	1.0000	1.0000	1.0000	1.0000	0.0000
.01	.9999	1.0000	1.0000	1.0000	.01728
.02	.9997	.9998	.9999	1.0000	.03455
.03	.9994	.9996	.9998	.9999	.05181
.04	.9989	.9992	.9997	.9998	.06905
.05	.9983	.9988	.9995	.9998	.08627
.06	.9975	.9982	.9993	.9996	.1035
.07	.9966	.9976	.9990	.9995	.1206
.08	.9955	.9968	.9987	.9994	.1377
.09	.9944	.9960	.9984	.9992	.1548
.10	.9930	.9950	.9980	.9990	.1718
.11	.9916	.9940	.9976	.9988	.1887
.12	.9900	.9928	.9971	.9986	.2056
.13	.9883	.9918	.9966	.9983	.2224
.14	.9864	.9903	.9961	.9980	.2391
.15	.9844	.9888	.9955	.9978	.2557
.16	.9823	.9873	.9949	.9974	.2723
.17	.9800	.9857	.9943	.9971	.2887
.18	.9776	.9840	.9936	.9968	.3051
.19	.9751	.9822	.9928	.9964	.3213
.20	.9725	.9803	.9921	.9960	.3374
.21	.9697	.9783	.9913	.9956	.3534
.22	.9668	.9762	.9904	.9952	.3693
.23	.9638	.9740	.9895	.9948	.3851
.24	.9607	.9718	.9886	.9943	.4007
.25	.9575	.9694	.9877	.9938	.4162
.26	.9541	.9670	.9867	.9933	.4315
.27	.9506	.9645	.9856	.9928	.4467
.28	.9470	.9619	.9846	.9923	.4618
.29	.9433	.9592	.9835	.9917	.4767
.30	.9395	.9564	.9823	.9911	.4914
.31	.9355	.9535	.9811	.9905	.5059
.32	.9315	.9506	.9799	.9899	.5203
.33	.9274	.9476	.9787	.9893	.5345
.34	.9231	.9445	.9774	.9886	.5486

TABLES

TABLE II (Continued)

Flow Parameters Versus M for Subsonic Flow

M	$p/p_0$	$\rho/\rho_0$	$T/T_0$	$a/a_0$	$A^*/A$
.35	.9188	.9413	.9761	.9880	.5624
.36	.9143	.9380	.9747	.9873	.5761
.37	.9098	.9347	.9733	.9866	.5896
.38	.9052	.9313	.9719	.9859	.6029
.39	.9004	.9278	.9705	.9851	.6160
.40	.8956	.9243	.9690	.9844	.6289
.41	.8907	.9207	.9675	.9836	.6416
.42	.8857	.9170	.9659	.9828	.6541
.43	.8807	.9132	.9643	.9820	.6663
.44	.8755	.9094	.9627	.9812	.6784
.45	.8703	.9055	.9611	.9803	.6903
.46	.8650	.9016	.9594	.9795	.7019
.47	.8597	.8976	.9577	.9786	.7134
.48	.8541	.8935	.9560	.9777	.7246
.49	.8486	.8894	.9542	.9768	.7356
.50	.8430	.8852	.9524	.9759	.7464
.51	.8374	.8809	.9506	.9750	.7569
.52	.8317	.8765	.9487	.9740	.7672
.53	.8259	.8723	.9468	.9730	.7773
.54	.8201	.8679	.9449	.9721	.7872
.55	.8142	.8634	.9430	.9711	.7968
.56	.8082	.8589	.9410	.9701	.8063
.57	.8022	.8544	.9390	.9690	.8155
.58	.7962	.8498	.9370	.9680	.8244
.59	.7901	.8451	.9349	.9669	.8331
.60	.7840	.8405	.9328	.9658	.8416
.61	.7778	.8357	.9307	.9647	.8499
.62	.7716	.8309	.9286	.9636	.8579
.63	.7654	.8262	.9265	.9625	.8657
.64	.7591	.8213	.9243	.9614	.8732
.65	.7528	.8164	.9221	.9603	.8806
.66	.7465	.8115	.9199	.9591	.8877
.67	.7401	.8066	.9176	.9579	.8945
.68	.7338	.8016	.9153	.9567	.9012
.69	.7274	.7966	.9131	.9555	.9076

TABLES

TABLE II (Continued)

Flow Parameters Versus M for Subsonic Flow

M	$p/p_0$	$\rho/\rho_0$	$T/T_0$	$a/a_0$	$A^*/A$
.70	.7209	.7916	.9107	.9443	.9138
.71	.7145	.7865	.9084	.9431	.9197
.72	.7080	.7814	.9061	.9419	.9254
.73	.7016	.7763	.9037	.9406	.9309
.74	.6951	.7712	.9013	.9394	.9362
.75	.6886	.7660	.8989	.9381	.9412
.76	.6821	.7609	.8964	.9368	.9461
.77	.6756	.7557	.8940	.9355	.9507
.78	.6690	.7505	.8915	.9342	.9551
.79	.6625	.7452	.8890	.9329	.9592
.80	.6560	.7400	.8865	.9316	.9632
.81	.6495	.7347	.8840	.9302	.9669
.82	.6430	.7295	.8815	.9289	.9704
.83	.6365	.7242	.8789	.9275	.9737
.84	.6300	.7189	.8763	.9261	.9769
.85	.6235	.7136	.8737	.9247	.9797
.86	.6170	.7083	.8711	.9232	.9824
.87	.6106	.7030	.8685	.9219	.9849
.88	.6041	.6977	.8659	.9205	.9872
.89	.5977	.6924	.8632	.9191	.9893
.90	.5913	.6870	.8606	.9177	.9912
.91	.5849	.6817	.8579	.9162	.9929
.92	.5785	.6764	.8552	.9148	.9944
.93	.5721	.6711	.8525	.9133	.9958
.94	.5658	.6658	.8498	.9118	.9969
.95	.5595	.6604	.8471	.9204	.9979
.96	.5532	.6551	.8444	.9189	.9986
.97	.5469	.6498	.8416	.9174	.9992
.98	.5407	.6445	.8389	.9159	.9997
.99	.5345	.6392	.8361	.9144	.9999
1.00	.5283	.6339	.8333	.9129	1.0000

Numerical values taken from NACA TN 1428, courtesy of the National Advisory Committee for Aeronautics. Set up from A. M. Kuethe and J. D. Schetzler, *Foundations of Aerodynamics*, John Wiley & Sons, New York, 1950.





TABLE III (Continued)

Flow Parameters Versus  $M$  for Supersonic Flow

$M$	$\frac{p}{p_0}$	$\frac{\rho}{\rho_0}$	$\frac{T}{T_0}$	$\frac{a}{a_0}$	$\frac{A^*}{A}$	$\frac{P}{P^*}$	$\frac{P}{P_0}$	$\frac{P}{P_0}$	$\theta$
2.05	.1182	.2176	.5433	.7371	.5682	.3478	.2775	2.40	27.75
2.06	.1164	.2152	.5409	.7355	.5634	.3458	28.02	2.41	28.02
2.07	.1146	.2128	.5385	.7338	.5586	.3437	28.29	2.42	28.29
2.08	.1128	.2104	.5361	.7322	.5538	.3417	28.56	2.43	28.56
2.09	.1111	.2081	.5337	.7306	.5491	.3396	28.83	2.44	28.83
2.10	.1094	.2058	.5313	.7290	.5444	.3376	29.10	2.45	29.10
2.11	.1077	.2035	.5290	.7273	.5397	.3355	29.36	2.46	29.36
2.12	.1060	.2013	.5266	.7257	.5350	.3334	29.63	2.47	29.63
2.13	.1043	.1990	.5243	.7241	.5304	.3314	29.90	2.48	29.90
2.14	.1027	.1968	.5219	.7225	.5258	.3293	30.16	2.49	30.16
2.15	.1011	.1946	.5196	.7208	.5212	.3272	30.43	2.50	30.43
2.16	.09956	.1925	.5173	.7192	.5167	.3252	30.69	2.51	30.69
2.17	.09802	.1903	.5150	.7176	.5122	.3231	30.95	2.52	30.95
2.18	.09650	.1882	.5127	.7160	.5077	.3210	31.21	2.53	31.21
2.19	.09500	.1861	.5104	.7144	.5032	.3189	31.47	2.54	31.47
2.20	.09352	.1841	.5081	.7128	.4988	.3169	31.73	2.55	31.73
2.21	.09207	.1820	.5059	.7112	.4944	.3148	31.99	2.56	31.99
2.22	.09064	.1800	.5036	.7097	.4900	.3127	32.25	2.57	32.25
2.23	.08923	.1780	.5014	.7081	.4856	.3106	32.51	2.58	32.51
2.24	.08785	.1760	.4991	.7065	.4813	.3085	32.76	2.59	32.76
2.25	.08648	.1740	.4969	.7049	.4770	.3065	33.02	2.60	33.02
2.26	.08514	.1721	.4947	.7033	.4727	.3044	33.27	2.61	33.27
2.27	.08382	.1702	.4925	.7018	.4685	.3023	33.53	2.62	33.53
2.28	.08252	.1683	.4903	.7002	.4643	.3003	33.78	2.63	33.78
2.29	.08123	.1664	.4881	.6986	.4601	.2982	34.03	2.64	34.03
2.30	.07997	.1646	.4859	.6971	.4560	.2961	34.28	2.65	34.28
2.31	.07873	.1628	.4837	.6955	.4519	.2941	34.53	2.66	34.53
2.32	.07751	.1609	.4816	.6940	.4478	.2920	34.78	2.67	34.78
2.33	.07631	.1592	.4794	.6924	.4437	.2900	35.03	2.68	35.03
2.34	.07512	.1574	.4773	.6909	.4397	.2879	35.28	2.69	35.28
2.35	.07396	.1556	.4752	.6893	.4357	.2859	35.53	2.70	35.53
2.36	.07281	.1539	.4731	.6878	.4317	.2839	35.77	2.71	35.77
2.37	.07168	.1522	.4709	.6863	.4278	.2818	36.02	2.72	36.02
2.38	.07057	.1505	.4688	.6847	.4239	.2798	36.26	2.73	36.26
2.39	.06948	.1488	.4668	.6832	.4200	.2778	36.50	2.74	36.50

TABLE III (Continued)

Flow Parameters Versus  $M$  for Supersonic Flow

$M$	$\frac{p}{p_0}$	$\frac{\rho}{\rho_0}$	$\frac{T}{T_0}$	$\frac{a}{a_0}$	$\frac{A^*}{A}$	$\frac{P}{P^*}$	$\frac{P}{P_0}$	$\frac{P}{P_0}$	$\theta$
2.40	.06840	.1472	.4647	.6817	.4161	.2758	36.75	2.75	36.75
2.41	.06734	.1456	.4626	.6802	.4123	.2738	36.99	2.76	36.99
2.42	.06630	.1439	.4606	.6786	.4085	.2718	37.23	2.77	37.23
2.43	.06527	.1424	.4585	.6771	.4048	.2698	37.47	2.78	37.47
2.44	.06426	.1408	.4565	.6756	.4010	.2678	37.71	2.79	37.71
2.45	.06327	.1392	.4544	.6741	.3973	.2658	37.95	2.80	37.95
2.46	.06229	.1377	.4524	.6726	.3937	.2639	38.18	2.81	38.18
2.47	.06133	.1362	.4504	.6711	.3900	.2619	38.42	2.82	38.42
2.48	.06038	.1347	.4484	.6696	.3864	.2599	38.66	2.83	38.66
2.49	.05945	.1332	.4464	.6681	.3828	.2580	38.89	2.84	38.89
2.50	.05853	.1317	.4444	.6667	.3793	.2561	39.12	2.85	39.12
2.51	.05762	.1302	.4425	.6652	.3757	.2541	39.36	2.86	39.36
2.52	.05674	.1288	.4405	.6637	.3722	.2522	39.59	2.87	39.59
2.53	.05586	.1274	.4386	.6622	.3686	.2503	39.82	2.88	39.82
2.54	.05500	.1260	.4366	.6608	.3653	.2484	40.05	2.89	40.05
2.55	.05415	.1246	.4347	.6593	.3619	.2465	40.28	2.90	40.28
2.56	.05332	.1232	.4328	.6579	.3585	.2446	40.51	2.91	40.51
2.57	.05250	.1218	.4309	.6564	.3552	.2427	40.75	2.92	40.75
2.58	.05169	.1205	.4289	.6549	.3519	.2409	40.96	2.93	40.96
2.59	.05090	.1192	.4271	.6535	.3486	.2390	41.19	2.94	41.19
2.60	.05012	.1179	.4252	.6521	.3453	.2371	41.41	2.95	41.41
2.61	.04935	.1166	.4233	.6506	.3421	.2353	41.64	2.96	41.64
2.62	.04859	.1153	.4214	.6492	.3389	.2335	41.86	2.97	41.86
2.63	.04784	.1140	.4196	.6477	.3357	.2317	42.09	2.98	42.09
2.64	.04711	.1128	.4177	.6463	.3325	.2298	42.31	2.99	42.31
2.65	.04639	.1115	.4159	.6449	.3294	.2280	42.53	3.00	42.53
2.66	.04568	.1103	.4141	.6435	.3263	.2262	42.75	3.01	42.75
2.67	.04498	.1091	.4122	.6421	.3232	.2245	42.97	3.02	42.97
2.68	.04429	.1079	.4104	.6406	.3202	.2227	43.19	3.03	43.19
2.69	.04362	.1067	.4086	.6392	.3172	.2209	43.40	3.04	43.40
2.70	.04295	.1056	.4068	.6378	.3142	.2192	43.62	3.05	43.62
2.71	.04229	.1044	.4051	.6364	.3112	.2174	43.84	3.06	43.84
2.72	.04165	.1033	.4033	.6350	.3083	.2157	44.05	3.07	44.05
2.73	.04102	.1022	.4015	.6337	.3054	.2140	44.27	3.08	44.27
2.74	.04039	.1010	.3998	.6323	.3025	.2123	44.48	3.09	44.48

TABLE III (Continued)

Flow Parameters Versus  $M$  for Supersonic Flow

$M$	$\frac{p}{p_0}$	$\frac{\rho}{\rho_0}$	$\frac{T}{T_0}$	$\frac{a}{a_0}$	$\frac{A^*}{A}$	$\frac{P}{P^*}$	$\frac{P}{P_0}$	$\frac{P}{P_0}$	$\theta$
2.75	.03978	.10994	.3980	.6309	.2996	.2106	44.69	3.05	44.69
2.76	.03917	.10885	.3963	.6295	.2968	.2089	44.91	3.06	44.91
2.77	.03858	.10778	.3945	.6281	.2940	.2072	45.12	3.07	45.12
2.78	.03799	.10671	.3928	.6268	.2912	.2055	45.33	3.08	45.33
2.79	.03742	.10566	.3911	.6254	.2884	.2039	45.54	3.09	45.54
2.80	.03685	.10463	.3894	.6240	.2857	.2022	45.75	3.10	45.75
2.81	.03629	.10360	.3877	.6227	.2830	.2006	45.95	3.11	45.95
2.82	.03574	.10259	.3860	.6213	.2803	.1990	46.16	3.12	46.16
2.83	.03520	.10158	.3844	.6200	.2777	.1973	46.37	3.13	46.37
2.84	.03467	.10059	.3827	.6186	.2750	.1957	46.57	3.14	46.57
2.85	.03415	.09962	.3810	.6173	.2724	.1941	46.78	3.15	46.78
2.86	.03363	.09865	.3794	.6159	.2698	.1926	46.98	3.16	46.98
2.87	.03312	.09769	.3777	.6146	.2673	.1910	47.19	3.17	47.19
2.88	.03263	.09675	.3761	.6133	.2648	.1894	47.39	3.18	47.39
2.89	.03213	.09581	.3745	.6119	.2622	.1879	47.59	3.19	47.59
2.90	.03165	.09489	.3729	.6106	.2598	.1863	47.79	3.20	47.79
2.91	.03118	.09398	.3712	.6093	.2573	.1848	47.99	3.21	47.99
2.92	.03071	.09307	.3696	.6080	.2549	.1833	48.19	3.22	48.19
2.93	.03025	.09218	.3681	.6067	.2524	.1818	48.39	3.23	48.39
2.94	.02980	.09130	.3665	.6054	.2500	.1803	48.59	3.24	48.59
2.95	.02935	.09043	.3649	.6041	.2477	.1788	48.78	3.25	48.78
2.96	.02891	.08957	.3633	.6028	.2453	.1773	48.98	3.26	48.98
2.97	.02848	.08872	.3618	.6015	.2430	.1758	49.18	3.27	49.18
2.98	.02805	.08788	.3602	.6002	.2407	.1744	49.37	3.28	49.37
2.99	.02764	.08705	.3587	.5989	.2384	.1729	49.56	3.29	49.56
3.00	.02722	.08623	.3571	.5976	.2362	.1715	49.76	3.30	49.76
3.01	.02682	.08541	.3556	.5963	.2339	.1701	49.95	3.31	49.95
3.02	.02642	.08461	.3541	.5951	.2317	.1687	50.14	3.32	50.14
3.03	.02603	.08382	.3526	.5938	.2295	.1673	50.33	3.33	50.33
3.04	.02564	.08303	.3511	.5925	.2273	.1659	50.52	3.34	50.52
3.05	.02526	.08226	.3496	.5913	.2252	.1645	50.71	3.35	50.71
3.06	.02489	.08151	.3481	.5900	.2230	.1631	50.90	3.36	50.90
3.07	.02453	.08077	.3466	.5887	.2209	.1618	51.09	3.37	51.09
3.08	.02416	.08004	.3452	.5875	.2188	.1604	51.28	3.38	51.28
3.09	.02380	.07925	.3437	.5862	.2168	.1591	51.46	3.39	51.46

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TABLE III (Continued)

Flow Parameters Versus  $M$  for Supersonic Flow

$M$	$\frac{p}{p_0}$	$\frac{\rho}{\rho_0}$	$\frac{T}{T_0}$	$\frac{a}{a_0}$	$\frac{A^*}{A}$	$\frac{P V^2}{p_0}$	$\theta$
3.10	.02346	.06852	.3422	.5850	.2147	.1577	51.65
3.11	.02310	.06779	.3408	.5838	.2127	.1564	51.84
3.12	.02276	.06708	.3393	.5825	.2107	.1551	52.02
3.13	.02243	.06637	.3379	.5813	.2087	.1538	52.20
3.14	.02210	.06568	.3365	.5801	.2067	.1525	52.39
3.15	.02177	.06499	.3351	.5788	.2048	.1512	52.57
3.16	.02146	.06430	.3337	.5776	.2028	.1500	52.75
3.17	.02114	.06363	.3323	.5764	.2009	.1487	52.93
3.18	.02083	.06296	.3309	.5752	.1990	.1475	53.11
3.19	.02053	.06231	.3295	.5740	.1971	.1462	53.29
3.20	.02023	.06165	.3281	.5728	.1953	.1450	53.47
3.21	.01993	.06101	.3267	.5716	.1934	.1438	53.65
3.22	.01964	.06037	.3253	.5704	.1916	.1426	53.83
3.23	.01936	.05975	.3240	.5692	.1898	.1414	54.00
3.24	.01908	.05912	.3226	.5680	.1880	.1402	54.18
3.25	.01880	.05851	.3213	.5668	.1863	.1390	54.35
3.26	.01853	.05790	.3199	.5656	.1845	.1378	54.53
3.27	.01826	.05730	.3186	.5645	.1828	.1367	54.71
3.28	.01799	.05671	.3173	.5633	.1810	.1355	54.88
3.29	.01773	.05612	.3160	.5621	.1793	.1344	55.05
3.30	.01748	.05554	.3147	.5609	.1777	.1332	55.22
3.31	.01722	.05497	.3134	.5598	.1760	.1321	55.39
3.32	.01698	.05440	.3121	.5586	.1743	.1310	55.56
3.33	.01673	.05384	.3108	.5575	.1727	.1299	55.73
3.34	.01649	.05329	.3095	.5563	.1711	.1288	55.90
3.35	.01625	.05274	.3082	.5552	.1695	.1277	56.07
3.36	.01602	.05220	.3069	.5540	.1679	.1266	56.24
3.37	.01579	.05166	.3057	.5529	.1663	.1255	56.41
3.38	.01557	.05113	.3044	.5517	.1648	.1245	56.58
3.39	.01534	.05060	.3032	.5506	.1632	.1234	56.75
3.40	.01513	.05009	.3019	.5495	.1617	.1224	56.91
3.41	.01491	.04958	.3007	.5484	.1602	.1214	57.07
3.42	.01470	.04908	.2995	.5472	.1587	.1203	57.24
3.43	.01449	.04858	.2982	.5461	.1572	.1193	57.40
3.44	.01428	.04808	.2970	.5450	.1558	.1183	57.56

TABLE III (Continued)

Flow Parameters Versus  $M$  for Supersonic Flow

$M$	$\frac{p}{p_0}$	$\frac{\rho}{\rho_0}$	$\frac{T}{T_0}$	$\frac{a}{a_0}$	$\frac{A^*}{A}$	$\frac{P V^2}{p_0}$	$\theta$
3.45	.01408	.04759	.2958	.5439	.1543	.1173	57.73
3.46	.01388	.04711	.2946	.5428	.1529	.1163	57.89
3.47	.01368	.04663	.2934	.5417	.1515	.1153	58.05
3.48	.01349	.04616	.2922	.5406	.1501	.1144	58.21
3.49	.01330	.04569	.2910	.5395	.1487	.1134	58.37
3.50	.01311	.04523	.2899	.5384	.1473	.1124	58.53
3.60	.01138	.04089	.2784	.5275	.1342	.1033	60.09
3.70	.01003	.03702	.2675	.5172	.1224	.09490	61.60
3.80	.00829	.03355	.2572	.5072	.1117	.08722	63.04
3.90	.00652	.03044	.2474	.4974	.1021	.08019	64.44
4.00	.00506	.02766	.2381	.4880	.09329	.07376	65.78
4.10	.00386	.02516	.2293	.4788	.08536	.06788	67.08
4.20	.00282	.02292	.2208	.4699	.07818	.06251	68.33
4.30	.00193	.02090	.2129	.4614	.07166	.05759	69.54
4.40	.00118	.01909	.2053	.4531	.06575	.05309	70.71
4.50	.00052	.01745	.1980	.4450	.06038	.04898	71.83
4.60	.00023	.01587	.1911	.4372	.05550	.04521	72.92
4.70	.00008	.01464	.1846	.4296	.05107	.04177	73.97
4.80	.00002	.01343	.1783	.4223	.04703	.03861	74.99
4.90	.00000	.01233	.1724	.4152	.04335	.03572	75.97
5.00	.00000	.01134	.1667	.4082	.04000	.03308	76.92
6.00	.00000	.00334	.1220	.3492	.01880	.01596	84.96
7.00	.00000	.00099	.00259	.3048	.00902	.00825	90.97
	$\times 10^{-4}$	$\times 10^{-3}$	$\times 10^{-3}$	$\times 10^{-3}$	$\times 10^{-3}$	$\times 10^{-3}$	

$M$	$\frac{p}{p_0}$	$\frac{\rho}{\rho_0}$	$\frac{T}{T_0}$	$\frac{a}{a_0}$	$\frac{A^*}{A}$	$\frac{P V^2}{p_0}$	$\theta$
8.00	1.024	1.414	.07246	.2692	5.260	4.589	95.02
9.00	4.739	8.150	.05814	.2411	3.056	2.087	99.32
10.00	2.356	4.948	.04762	.2182	1.866	1.649	102.3
100.00	2.790	5.983	4.998	.02236	2.157	1.953	127.0
$\infty$	$\times 10^{-12}$	$\times 10^{-9}$	$\times 10^{-4}$	0	$\times 10^{-8}$	$\times 10^{-8}$	130.5

Numerical values taken from NACA TN 1428, courtesy of the National Advisory Committee for Aeronautics. Setup from A. M. Kuethe and J. D. Schitzer, *Foundations of Aerodynamics*, John Wiley & Sons, New York, 1950.

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TABLE IV  
PARAMETERS FOR SHOCK FLOW

$M_1$	$p_2/p_1$	$p_2/p_1$	$T_2/T_1$	$a_2/a_1$	$p_2^0/p_1^0$	$M_2$ for Normal Shocks Only	$M_1$	$p_2/p_1$	$a_2/p_1$	$T_2/T_1$	$a_2/a_1$	$p_2^0/p_1^0$	$M_2$ for Normal Shocks Only	$M_1$	$p_2/p_1$	$a_2/p_1$	$T_2/T_1$	$a_2/a_1$	$p_2^0/p_1^0$	$M_2$ for Normal Shocks Only	$M_1$	$p_2/p_1$	$a_2/p_1$	$T_2/T_1$	$a_2/a_1$	$p_2^0/p_1^0$	$M_2$ for Normal Shocks Only
1.00	1.000	1.000	1.000	1.000	1.0000	1.0000	1.35	1.960	1.603	1.223	1.106	.9697	.7018	1.70	3.205	2.198	1.458	1.208	.8557	.6405							
1.01	1.023	1.017	1.007	1.003	1.0000	.9901	1.36	1.991	1.620	1.229	1.109	.9676	.7572	1.71	3.245	2.214	1.466	1.211	.8516	.6380							
1.02	1.047	1.033	1.013	1.007	1.0000	.9805	1.37	2.023	1.638	1.235	1.111	.9653	.7627	1.72	3.285	2.230	1.473	1.214	.8474	.6355							
1.03	1.071	1.050	1.020	1.010	1.0000	.9712	1.38	2.055	1.655	1.242	1.114	.9630	.7683	1.73	3.325	2.247	1.480	1.217	.8431	.6330							
1.04	1.095	1.067	1.026	1.013	.9999	.9620	1.39	2.087	1.672	1.248	1.117	.9606	.7740	1.74	3.366	2.263	1.487	1.220	.8389	.6305							
1.05	1.120	1.084	1.033	1.016	.9999	.9531	1.40	2.120	1.690	1.255	1.120	.9582	.7807	1.75	3.406	2.279	1.495	1.223	.8346	.6281							
1.06	1.144	1.101	1.039	1.019	.9998	.9444	1.41	2.153	1.707	1.261	1.123	.9557	.7855	1.76	3.447	2.295	1.502	1.226	.8302	.6257							
1.07	1.169	1.118	1.046	1.023	.9996	.9360	1.42	2.186	1.724	1.268	1.126	.9531	.7914	1.77	3.488	2.311	1.509	1.229	.8259	.6234							
1.08	1.194	1.135	1.052	1.026	.9994	.9277	1.43	2.219	1.742	1.274	1.129	.9504	.7974	1.78	3.530	2.327	1.517	1.232	.8215	.6210							
1.09	1.219	1.152	1.059	1.029	.9992	.9196	1.44	2.253	1.759	1.281	1.132	.9476	.8035	1.79	3.571	2.343	1.524	1.235	.8171	.6188							
1.10	1.245	1.169	1.065	1.032	.9989	.9118	1.45	2.286	1.776	1.287	1.135	.9448	.8096	1.80	3.613	2.359	1.532	1.238	.8127	.6165							
1.11	1.271	1.186	1.071	1.035	.9986	.9041	1.46	2.320	1.793	1.294	1.137	.9420	.8157	1.81	3.655	2.375	1.539	1.241	.8082	.6143							
1.12	1.297	1.203	1.078	1.038	.9982	.8966	1.47	2.354	1.811	1.300	1.140	.9390	.8210	1.82	3.698	2.391	1.547	1.244	.8038	.6121							
1.13	1.323	1.221	1.084	1.041	.9978	.8892	1.48	2.389	1.828	1.307	1.143	.9360	.8269	1.83	3.740	2.407	1.554	1.247	.7993	.6099							
1.14	1.350	1.238	1.090	1.044	.9973	.8820	1.49	2.423	1.845	1.314	1.146	.9329	.8329	1.84	3.783	2.422	1.562	1.250	.7948	.6078							
1.15	1.376	1.255	1.097	1.047	.9967	.8750	1.50	2.458	1.862	1.320	1.149	.9298	.8384	1.85	3.826	2.438	1.569	1.253	.7902	.6057							
1.16	1.403	1.272	1.103	1.050	.9961	.8682	1.51	2.493	1.879	1.327	1.152	.9266	.8441	1.86	3.870	2.454	1.577	1.256	.7857	.6036							
1.17	1.430	1.290	1.109	1.053	.9953	.8615	1.52	2.529	1.896	1.334	1.155	.9233	.8497	1.87	3.913	2.469	1.585	1.259	.7811	.6016							
1.18	1.458	1.307	1.115	1.056	.9946	.8549	1.53	2.564	1.913	1.340	1.158	.9200	.8554	1.88	3.957	2.485	1.592	1.262	.7765	.5996							
1.19	1.485	1.324	1.122	1.059	.9937	.8485	1.54	2.600	1.930	1.347	1.161	.9166	.8611	1.89	4.001	2.500	1.600	1.265	.7720	.5976							
1.20	1.513	1.342	1.128	1.062	.9928	.8422	1.55	2.636	1.947	1.354	1.164	.9132	.8668	1.90	4.045	2.516	1.608	1.268	.7674	.5956							
1.21	1.541	1.359	1.134	1.065	.9918	.8360	1.56	2.673	1.964	1.361	1.166	.9097	.8725	1.91	4.089	2.531	1.616	1.271	.7628	.5937							
1.22	1.570	1.376	1.141	1.068	.9907	.8300	1.57	2.709	1.981	1.367	1.169	.9061	.8782	1.92	4.134	2.546	1.624	1.274	.7581	.5918							
1.23	1.598	1.394	1.147	1.071	.9896	.8241	1.58	2.746	1.998	1.374	1.172	.9025	.8839	1.93	4.179	2.562	1.631	1.277	.7535	.5899							
1.24	1.627	1.411	1.153	1.074	.9884	.8183	1.59	2.783	2.015	1.381	1.175	.8989	.8896	1.94	4.224	2.577	1.639	1.280	.7488	.5880							
1.25	1.656	1.429	1.159	1.077	.9871	.8126	1.60	2.820	2.032	1.388	1.178	.8952	.8952	1.95	4.270	2.592	1.647	1.283	.7442	.5862							
1.26	1.686	1.446	1.166	1.080	.9857	.8071	1.61	2.857	2.049	1.395	1.181	.8914	.9009	1.96	4.316	2.607	1.655	1.287	.7395	.5844							
1.27	1.715	1.463	1.172	1.083	.9842	.8016	1.62	2.895	2.065	1.402	1.184	.8877	.9065	1.97	4.361	2.622	1.663	1.290	.7349	.5826							
1.28	1.745	1.481	1.178	1.085	.9827	.7963	1.63	2.933	2.082	1.409	1.187	.8838	.9123	1.98	4.407	2.637	1.671	1.293	.7302	.5808							
1.29	1.775	1.498	1.185	1.088	.9811	.7911	1.64	2.971	2.099	1.416	1.190	.8799	.9180	1.99	4.453	2.652	1.679	1.296	.7255	.5791							
1.30	1.805	1.516	1.191	1.091	.9794	.7860	1.65	3.010	2.115	1.423	1.193	.8760	.9237	2.00	4.500	2.667	1.688	1.299	.7209	.5773							
1.31	1.835	1.533	1.197	1.094	.9776	.7810	1.66	3.048	2.132	1.430	1.196	.8720	.9294	2.01	4.547	2.681	1.696	1.302	.7162	.5757							
1.32	1.866	1.551	1.204	1.097	.9758	.7760	1.67	3.087	2.148	1.437	1.199	.8680	.9351	2.02	4.594	2.696	1.704	1.305	.7115	.5740							
1.33	1.897	1.568	1.210	1.100	.9738	.7712	1.68	3.126	2.165	1.444	1.202	.8640	.9408	2.03	4.641	2.711	1.712	1.308	.7069	.5723							
1.34	1.928	1.585	1.216	1.103	.9718	.7664	1.69	3.165	2.181	1.451	1.205	.8599	.9461	2.04	4.689	2.725	1.720	1.312	.7022	.5707							

TABLES

TABLE IV (Continued)  
PARAMETERS FOR SHOCK FLOW

TABLES

TABLE IV (Continued)  
PARAMETERS FOR SHOCK FLOW

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TABLE IV (Continued)  
PARAMETERS FOR SHOCK FLOW

TABLE IV (Continued)  
PARAMETERS FOR SHOCK FLOW

TABLE IV (Continued)  
PARAMETERS FOR SHOCK FLOW

$M_1$	$p_2/p_1$	$T_2/T_1$	$a_2/a_1$	$p_2^0/p_1^0$	$M_2$ for Normal Shocks Only	$M_1$	$p_2/p_1$	$T_2/T_1$	$a_2/a_1$	$p_2^0/p_1^0$	$M_2$ For Normal Shocks On	$M_1$	$p_2/p_1$	$T_2/T_1$	$a_2/a_1$	$p_2^0/p_1^0$	$M_2$ For Normal Shocks Only
2.05	4.736	2.740	1.729	1.315	.6975	2.40	6.558	2.040	1.428	.5401	.5231	2.75	8.656	2.397	1.548	.4062	.4918
2.06	4.784	2.755	1.737	1.318	.6928	2.41	6.609	2.050	1.432	.5359	.5221	2.76	8.721	2.407	1.552	.4028	.4911
2.07	4.832	2.769	1.745	1.321	.6882	2.42	6.666	2.059	1.435	.5317	.5210	2.77	8.785	2.418	1.555	.3994	.4903
2.08	4.881	2.783	1.754	1.324	.6836	2.43	6.722	2.069	1.438	.5276	.5200	2.78	8.850	2.429	1.559	.3961	.4896
2.09	4.929	2.798	1.762	1.327	.6789	2.44	6.779	2.079	1.442	.5234	.5189	2.79	8.915	2.440	1.562	.3928	.4889
2.10	4.978	2.812	1.770	1.331	.6742	2.45	6.836	2.088	1.445	.5193	.5179	2.80	8.980	2.451	1.566	.3895	.4882
2.11	5.027	2.826	1.779	1.334	.6696	2.46	6.894	2.098	1.449	.5152	.5169	2.81	9.045	2.462	1.569	.3862	.4875
2.12	5.077	2.840	1.787	1.337	.6649	2.47	6.951	2.108	1.452	.5111	.5159	2.82	9.111	2.473	1.573	.3829	.4868
2.13	5.126	2.854	1.796	1.340	.6603	2.48	7.009	2.118	1.455	.5071	.5149	2.83	9.177	2.484	1.576	.3797	.4861
2.14	5.176	2.868	1.805	1.343	.6557	2.49	7.067	2.128	1.459	.5030	.5140	2.84	9.243	2.496	1.580	.3765	.4854
2.15	5.226	2.882	1.813	1.347	.6511	2.50	7.125	2.138	1.462	.4990	.5130	2.85	9.310	2.507	1.583	.3733	.4847
2.16	5.277	2.896	1.822	1.350	.6464	2.51	7.183	2.147	1.465	.4950	.5120	2.86	9.376	2.518	1.587	.3701	.4840
2.17	5.327	2.910	1.831	1.353	.6419	2.52	7.242	2.157	1.468	.4911	.5111	2.87	9.443	2.529	1.590	.3670	.4833
2.18	5.378	2.924	1.839	1.356	.6373	2.53	7.301	2.167	1.472	.4871	.5102	2.88	9.510	2.540	1.594	.3639	.4827
2.19	5.429	2.938	1.848	1.359	.6327	2.54	7.360	2.177	1.476	.4832	.5092	2.89	9.577	2.552	1.597	.3608	.4820
2.20	5.480	2.951	1.857	1.363	.6281	2.55	7.420	2.187	1.479	.4793	.5083	2.90	9.645	2.563	1.601	.3577	.4814
2.21	5.531	2.965	1.866	1.366	.6236	2.56	7.479	2.198	1.482	.4754	.5074	2.91	9.713	2.575	1.605	.3547	.4807
2.22	5.583	2.978	1.875	1.369	.6191	2.57	7.539	2.208	1.486	.4715	.5065	2.92	9.781	2.586	1.608	.3517	.4801
2.23	5.635	2.992	1.883	1.372	.6145	2.58	7.599	2.218	1.489	.4677	.5056	2.93	9.849	2.598	1.612	.3487	.4795
2.24	5.687	3.005	1.892	1.376	.6100	2.59	7.659	2.228	1.493	.4639	.5047	2.94	9.918	2.609	1.615	.3457	.4788
2.25	5.740	3.019	1.901	1.379	.6055	2.60	7.720	2.238	1.496	.4601	.5039	2.95	9.986	2.621	1.619	.3428	.4782
2.26	5.792	3.032	1.910	1.382	.6011	2.61	7.781	2.249	1.500	.4564	.5030	2.96	10.06	2.632	1.622	.3398	.4776
2.27	5.845	3.045	1.919	1.385	.5966	2.62	7.842	2.259	1.503	.4526	.5022	2.97	10.12	2.644	1.626	.3369	.4770
2.28	5.898	3.058	1.929	1.389	.5921	2.63	7.903	2.269	1.506	.4489	.5013	2.98	10.19	2.656	1.630	.3340	.4764
2.29	5.951	3.071	1.938	1.392	.5877	2.64	7.965	2.280	1.510	.4452	.5005	2.99	10.26	2.667	1.633	.3312	.4758
2.30	6.005	3.085	1.947	1.395	.5833	2.65	8.026	2.290	1.513	.4416	.4996	3.00	10.33	2.679	1.637	.3283	.4752
2.31	6.059	3.098	1.956	1.399	.5789	2.66	8.088	2.301	1.517	.4379	.4988	3.10	11.05	2.799	1.673	.3012	.4695
2.32	6.113	3.110	1.965	1.402	.5745	2.67	8.150	2.311	1.520	.4343	.4980	3.20	11.78	2.922	1.709	.2762	.4633
2.33	6.167	3.123	1.974	1.405	.5702	2.68	8.213	2.322	1.524	.4307	.4972	3.30	12.52	3.049	1.746	.2533	.4590
2.34	6.222	3.136	1.984	1.408	.5658	2.69	8.275	2.332	1.527	.4271	.4964	3.40	13.34	3.180	1.783	.2322	.4552
2.35	6.276	3.149	1.993	1.412	.5615	2.70	8.338	2.343	1.531	.4236	.4956	3.50	14.13	3.315	1.821	.2129	.4512
2.36	6.331	3.162	2.002	1.415	.5572	2.71	8.401	2.354	1.534	.4201	.4949	3.60	14.95	3.454	1.858	.1953	.4474
2.37	6.386	3.174	2.012	1.418	.5529	2.72	8.465	2.364	1.538	.4166	.4941	3.70	15.80	3.596	1.896	.1792	.4439
2.38	6.442	3.187	2.021	1.422	.5486	2.73	8.528	2.375	1.541	.4131	.4933	3.80	16.68	3.743	1.935	.1645	.4407
2.39	6.497	3.199	2.031	1.425	.5444	2.74	8.592	2.386	1.545	.4097	.4926	3.90	17.58	3.893	1.973	.1510	.4377

TABLES

TABLE IV (Continued)  
PARAMETERS FOR SHOCK FLOW

$M_b$	$p_0/p_1$	$p_0/p_1$	$T_2/T_1$	$a_2/a_1$	$p_2^0/p_1^0$	$M_2$ for Normal Shocks Only
4.00	18.50	4.571	4.047	2.012	.1388	.4350
5.00	29.00	5.000	5.800	2.408	.06172	.4152
6.00	41.83	5.288	7.941	2.818	.02965	.4042
7.00	57.00	5.464	10.47	3.236	.01535	.3974
8.00	75.60	5.565	13.39	3.659	8.488 × 10 <sup>-3</sup>	.3929
9.00	94.33	5.651	16.69	4.086	4.904 × 10 <sup>-3</sup>	.3898
10.00	116.5	5.714	20.39	4.515	3.045 × 10 <sup>-3</sup>	.3876
100.00	11,686.5	5.907	1945.4	44.11	3.593 × 10 <sup>-8</sup>	.3781
∞	∞	6	∞	∞	0	.3780

Data taken from NACA TN 1428, courtesy of National Advisory Committee of Aeronautics. Setup from A. M. Kuethe and J. D. Schetzler, *Foundations of Aerodynamics*, John Wiley & Sons, New York, 1950.

TABLES

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TABLE V  
MACH NUMBER AND MACH ANGLE VERSUS PRANDTL-MEYER FUNCTION

$\nu$ (deg)	$M$	$\mu$ (deg)	$\nu$ (deg)	$M$	$\mu$ (deg)
0.0	1.000	90.000	17.5	1.689	36.293
0.5	1.051	72.099	18.0	1.706	35.874
1.0	1.082	67.574	18.5	1.724	35.465
1.5	1.108	64.451	19.0	1.741	35.065
2.0	1.133	61.997	19.5	1.758	34.673
2.5	1.155	59.950	20.0	1.775	34.290
3.0	1.177	58.180	20.5	1.792	33.915
3.5	1.198	56.614	21.0	1.810	33.548
4.0	1.218	55.205	21.5	1.827	33.188
4.5	1.237	53.920	22.0	1.844	32.834
5.0	1.256	52.738	22.5	1.862	32.488
5.5	1.275	51.642	23.0	1.879	32.148
6.0	1.294	50.619	23.5	1.897	31.814
6.5	1.312	49.658	24.0	1.915	31.486
7.0	1.330	48.753	24.5	1.932	31.164
7.5	1.348	47.896	25.0	1.950	30.847
8.0	1.366	47.082	25.5	1.968	30.536
8.5	1.383	46.306	26.0	1.986	30.229
9.0	1.400	45.566	26.5	2.004	29.928
9.5	1.418	44.857	27.0	2.023	29.632
10.0	1.435	44.177	27.5	2.041	29.340
10.5	1.452	43.523	28.0	2.059	29.052
11.0	1.469	42.894	28.5	2.078	28.769
11.5	1.486	42.287	29.0	2.096	28.491
12.0	1.503	41.701	29.5	2.115	28.216
12.5	1.520	41.134	30.0	2.134	27.945
13.0	1.537	40.585	30.5	2.153	27.678
13.5	1.554	40.053	31.0	2.172	27.415
14.0	1.571	39.537	31.5	2.191	27.155
14.5	1.588	39.035	32.0	2.210	26.899
15.0	1.605	38.547	32.5	2.230	26.646
15.5	1.622	38.073	33.0	2.249	26.397
16.0	1.639	37.611	33.5	2.269	26.151
16.5	1.655	37.160	34.0	2.289	25.908
17.0	1.672	36.721	34.5	2.309	25.668

TABLES

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TABLE V (Continued)

MACH NUMBER AND MACH ANGLE VERSUS PRANDTL-MEYER FUNCTION

$\nu$ (deg)	$M$	$\mu$ (deg)	$\nu$ (deg)	$M$	$\mu$ (deg)
35.0	2.329	25.430	52.5	3.146	18.532
35.5	2.349	25.196	53.0	3.174	18.366
36.0	2.369	24.965	53.5	3.202	18.200
36.5	2.390	24.736	54.0	3.230	18.036
37.0	2.410	24.510	54.5	3.258	17.873
37.5	2.431	24.287	55.0	3.287	17.711
38.0	2.452	24.066	55.5	3.316	17.551
38.5	2.473	23.847	56.0	3.346	17.391
39.0	2.495	23.631	56.5	3.375	17.233
39.5	2.516	23.418	57.0	3.406	17.076
40.0	2.538	23.206	57.5	3.436	16.920
40.5	2.560	22.997	58.0	3.467	16.765
41.0	2.582	22.790	58.5	3.498	16.611
41.5	2.604	22.582	59.0	3.530	16.458
42.0	2.626	22.382	59.5	3.562	16.306
42.5	2.649	22.182	60.0	3.594	16.155
43.0	2.671	21.983	60.5	3.627	16.005
43.5	2.694	21.786	61.0	3.660	15.856
44.0	2.718	21.591	61.5	3.694	15.708
44.5	2.741	21.398	62.0	3.728	15.561
45.0	2.764	21.207	62.5	3.762	15.415
45.5	2.788	21.017	63.0	3.797	15.270
46.0	2.812	20.830	63.5	3.832	15.126
46.5	2.836	20.644	64.0	3.868	14.983
47.0	2.861	20.459	64.5	3.904	14.840
47.5	2.886	20.277	65.0	3.941	14.698
48.0	2.910	20.096	65.5	3.979	14.557
48.5	2.936	19.916	66.0	4.016	14.417
49.0	2.961	19.738	66.5	4.055	14.278
49.5	2.987	19.561	67.0	4.094	14.140
50.0	3.013	19.386	67.5	4.133	14.002
50.5	3.039	19.213	68.0	4.173	13.865
51.0	3.065	19.041	68.5	4.214	13.729
51.5	3.092	18.870	69.0	4.255	13.593
52.0	3.119	18.701	69.5	4.297	13.459

TABLES

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TABLE V (Continued)

MACH NUMBER AND MACH ANGLE VERSUS PRANDTL-MEYER FUNCTION

$\nu$ (deg)	$M$	$\mu$ (deg)	$\nu$ (deg)	$M$	$\mu$ (deg)
70.0	4.339	13.325	87.5	6.390	9.003
70.5	4.382	13.191	88.0	6.472	8.888
71.0	4.426	13.059	88.5	6.556	8.774
71.5	4.470	12.927	89.0	6.642	8.660
72.0	4.515	12.795	89.5	6.729	8.546
72.5	4.561	12.665	90.0	6.819	8.433
73.0	4.608	12.535	90.5	6.911	8.320
73.5	4.655	12.406	91.0	7.005	8.207
74.0	4.703	12.277	91.5	7.102	8.095
74.5	4.752	12.149	92.0	7.201	7.983
75.0	4.801	12.021	92.5	7.302	7.871
75.5	4.852	11.894	93.0	7.406	7.760
76.0	4.903	11.768	93.5	7.513	7.649
76.5	4.955	11.642	94.0	7.623	7.538
77.0	5.009	11.517	94.5	7.735	7.428
77.5	5.063	11.392	95.0	7.851	7.318
78.0	5.118	11.268	95.5	7.970	7.208
78.5	5.174	11.145	96.0	8.092	7.099
79.0	5.231	11.022	96.5	8.218	6.989
79.5	5.289	10.899	97.0	8.347	6.881
80.0	5.348	10.777	97.5	8.480	6.772
80.5	5.408	10.656	98.0	8.618	6.664
81.0	5.470	10.535	98.5	8.759	6.556
81.5	5.532	10.414	99.0	8.905	6.448
82.0	5.596	10.294	99.5	9.055	6.340
82.5	5.661	10.175	100.0	9.210	6.233
83.0	5.727	10.056	100.5	9.371	6.126
83.5	5.795	9.937	101.0	9.536	6.019
84.0	5.864	9.819	101.5	9.708	5.913
84.5	5.935	9.701	102.0	9.885	5.806
85.0	6.006	9.584			
85.5	6.080	9.467			
86.0	6.155	9.350			
86.5	6.232	9.234			
87.0	6.310	9.119			

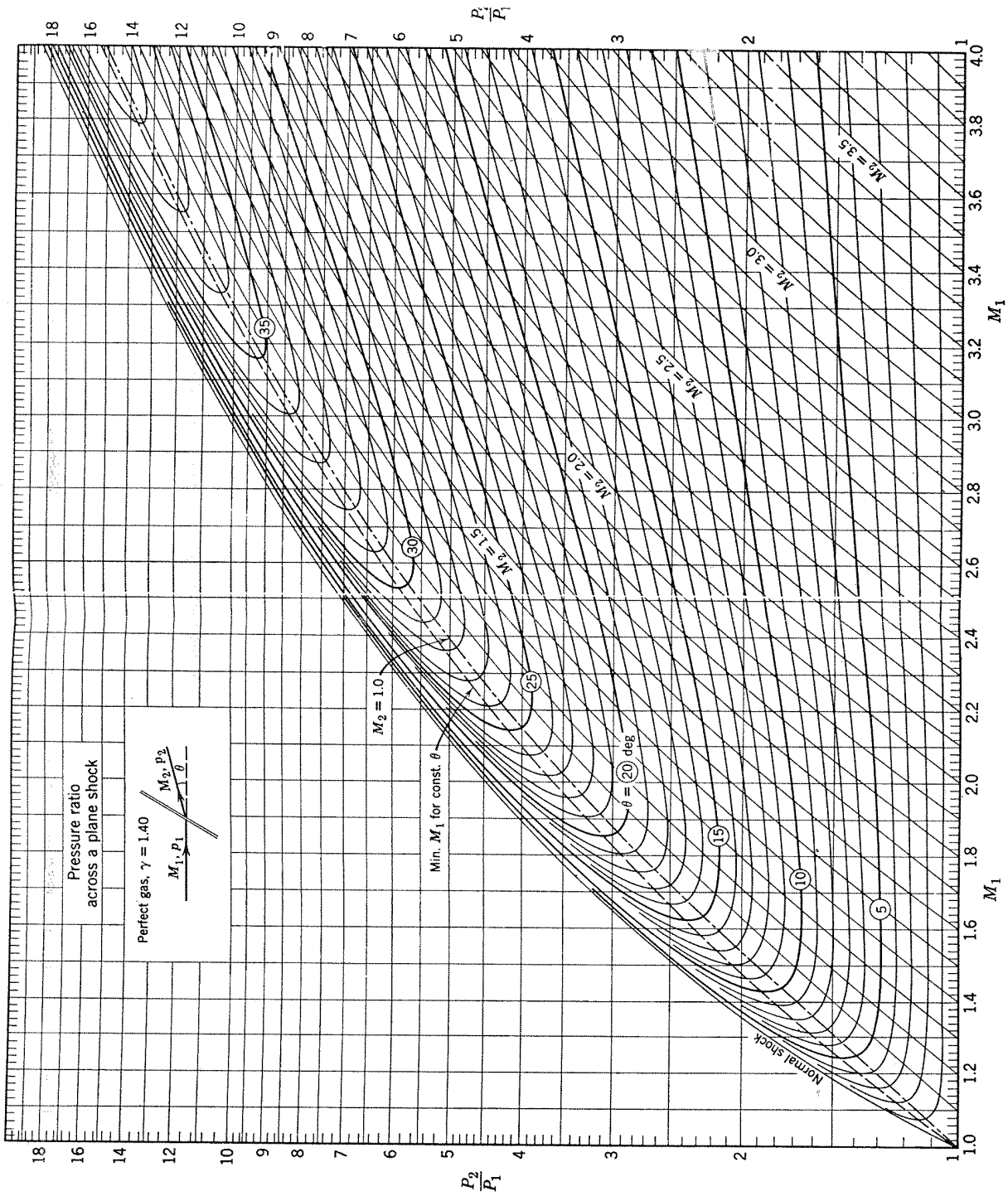


CHART 2 (continued)

OBLIQUE SHOCK CHART 2 Variation of pressure ratio and downstream Mach number with flow-deflection angle and upstream Mach number. (Data from C. L. Dailey and F. C. Wood, *Computation Curves for Compressible Flow Problems*, Wiley, 1949.)